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THERMODYNAMIC STUDY OF ALLOYS BY E.M.F. MEASUREMENTS:
THEORY AND APPLICATION TO LIQUID LANTHANUM-ZINC ALLOYS

by



JEAN-BAPTISTE P.F. LESOURD

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of

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The undersigned certify that they have read, and recommend to the Faculty of Graduate Studies for acceptance, a thesis entitled:

"THERMODYNAMIC STUDY OF ALLOYS BY E.M.F.
MEASUREMENTS: THEORY AND APPLICATION TO
LIQUID LANTHANUM-ZINC ALLOYS"

submitted by JEAN-BAPTISTE P.F. LESOURD, in partial fulfilment of the requirements for the degree of Master of Science.

A B S T R A C T

The historical and theoretical backgrounds for thermodynamic studies of alloys by e.m.f. methods have been surveyed. The published theoretical thermodynamic studies on multicomponent systems, of particular interest in the case of multicomponent alloys investigated by e.m.f. methods, have been reviewed and some of the equations rederived.

The case of e.m.f. studies on binary zinc alloys has been reviewed.

The e.m.f. of cells of the type $\text{La(s)}/\text{LiCl-KCl (eutectic)} - \text{LaCl}_3/(\text{La} - \text{Zn, saturated liquid alloy})$ has been measured over the temperature range 450-600°C. Thermodynamic functions for the limiting lanthanum-zinc solid intermetallic compound existing in this range are: ΔG_f° , -58.8 kcal/mole; ΔS_f° , -53 cal/deg-mole; ΔH_f° , -97 kcal/mole at 450°C. The standard potential of the $\text{La(III)}/\text{La(0)}$ couple was measured at 450°C as -2.883 V, mole fraction scale and $\text{Pt(II)}/\text{Pt(0)}$ reference. The significance of these measurements for the electrochemical separation of lanthanum and uranium is discussed.

A C K N O W L E D G E M E N T S

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L I S T O F S Y M B O L S

- A: Coefficient in representation of regular solutions.
- a,b: Integration limits.
- a (with subscript): Activity (of subscripted component).
- c: Number of components.
- E: Electromotive force (e.m.f.).
- F: Helmholtz free energy (U-TS).
- F: Faraday constant.
- f: Function of c-1 variables.
- G: Gibbs free energy (H-TS, referred to as "free energy").
- H: Enthalpy.
- L: Limit.
- n: Oxidation state or charge of ion.
- n (with subscript): Number of moles (of subscripted component).
- P: Pressure.
- R: Gas constant.
- S: Entropy.
- T: Absolute temperature.
- U: Energy.
- V: Volume.
- w. Solubility (g/kg).
- x (with subscript): Mole fraction (of subscripted component).
- Z: Thermodynamic property (general).
- z: (with or without subscript): Integral or partial molal value (for subscripted component) of Z. Small letters (with or without subscript) are also used for other extensive thermodynamic properties, such as G, H and S, to denote integral or partial molal values (for subscripted component) of these properties.

α : Lagrange multiplier.

γ (with subscript): Activity coefficient (of subscripted component).

$\Delta G, \Delta H, \Delta S$: Variations of G, H, S .

$\Delta x_1, \Delta x_2$: Difference between mole fractions in the liquid and the solid phase for components 1 and 2.

λ : Arbitrary number.

λ (with subscript): Variable describing the composition of a multicomponent system (subscript may or may not refer to a particular component).

μ (with subscript): Chemical potential (of subscripted component).

Subscripts

f : Refers to the variation of formation of a thermodynamic property for the compound following between brackets.

i, j, k , or specific integral number or chemical symbol:

Refers to a particular component.

o : Refers to a specific point (temperature, composition).

Superscripts

e : Refers to a change of excess.

m : Refers to a change of mixing.

o : Refers to a standard or reference state.

Other notations

e (between brackets): Refers to a eutectic point.

l (between brackets): Refers to the liquid state.

s (between brackets): Refers to the solid state.

M (with or without subscript): Chemical symbol.

B_1 , B_2 , C_1 , C_2 , I, P(l), P(s): Points in figure 2,
defined in text.

The meaning of other symbols used is the generally
accepted meaning.

I. INTRODUCTION

This work is concerned with the study of thermodynamic properties of alloys by electrochemical methods, in general and in the particular case of liquid lanthanum-zinc alloys.

I-1. Historical survey

Within the earliest studies of alloys by e.m.f. methods were the investigation on amalgams by two German scientists, Von Türlin¹ and Meyer², in 1890 and 1891. They expected to find the molecular masses of the metals dissolved in mercury from the e.m.f. between two amalgams of the same metal, at different concentrations. In 1898, Cady³ showed that this was not a satisfactory method for the determination of molecular masses of solutes in mercury, and tried to explain deviations from ideality. Numerous e.m.f. studies on amalgams were made until 1920, in Germany⁴⁻⁶ and in the United States, particularly by G. N. Lewis and his coworkers⁷⁻¹⁰, who were able to calculate indirectly standard potentials for the alkali metals in water by using amalgam cells. Their work is still the best available on standard potentials of alkali metals. The cells used in such experiments were composed of two amalgams of different concentrations in a given metal as electrodes, and a solution of one of the ions

of this metal in water or an ionizing organic solvent as electrolyte (since mercury is seldom less noble than its solute, the electrolyte is a solution of one of the ions of the solute rather than of mercury). In 1921, G. N. Lewis¹¹ interpreted the results of Richards and Daniels¹² concerning the e.m.f. of concentrated thallium amalgam cells in terms of activities. Two years later, in 1923, Gerke¹³ reviewed the previous work on amalgams and used the saturated amalgam data to calculate the free energies of formation of intermetallic compounds of mercury. At this date¹⁴, investigators started using molten salts as conductors, thus permitting the study of alloys at higher temperatures. Both liquid alloys¹⁵⁻¹⁸ and solid alloys¹⁹⁻²¹ have been the object of a large number of e.m.f. experiments since then. This subject has been reviewed²²⁻²⁶; e.m.f. studies of binary zinc alloys are reviewed here. The concept of regular solution, introduced in 1935 by Hildebrand²⁷, was found useful for the interpretation of experimental results in intermetallic solutions. Simultaneously, Seltz²⁸⁻³⁰ applied e.m.f. measurements in alloy systems to the determination of binary diagrams. A further theoretical advance is due to Darken³¹ who, in 1950, obtained general thermodynamic equations for ternary and multicomponent systems. The theory of Darken has been modified and generalized³²⁻³⁴.

It has been applied to ternary alloys ³⁵⁻³⁹.

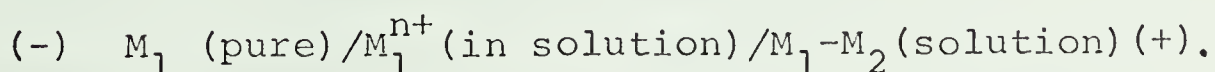
Since 1950, other advances occurred in experimental methods; molten salt techniques were improved, particularly as far as purification is concerned ⁴⁰⁻⁴². Solid electrolytes, such as glasses ⁴³, and non-ionic conductors ^{44,45} have been used.

I-2. E.m.f. measurements in binary alloys and directly related data.

The e.m.f. methods of study of a binary alloy between two metals involve e.m.f. measurements in cells such as:

Reference electrode/ionic conductor/ M_1 - M_2 (alloy).

There are indeed many possibilities for the choice of the reference electrode and the conductor. One of the most convenient choices for the reference electrode is one of the pure components of the alloy, such as M_1 , and for the conductor, an ionic conductor containing an ion of M_1 , of charge n , M_1^{n+} . This choice is convenient because then the terms related to the ionic concentrations vanish, and the e.m.f. is characteristic of the alloy only. This discussion shall be restricted to this case, i.e. to cells of the form:



In order that this method yield reliable and easily interpretable data, the following conditions have to be fulfilled:

(a) M_1 is dissolved spontaneously in the M_1 - M_2 solution, which means that the M_1 electrode is the anode (-) and that the M_1 - M_2 solution is the cathode (+). In other terms, the free energy of formation of the M_1 - M_2 solution has to be negative, otherwise no such solution can exist.

(b) The electrode processes which take place involve M_1 and M_1 only. M_1 must, therefore, be the more electropositive metal present, otherwise the M_1^{n+} cations would be reduced by the more electropositive metal M_2 . Difficulties are likely to be encountered if M_1 and M_2 are not far enough from each other in the electrode potential series for the solvent being used. This point has been discussed quantitatively by Wagner and Werner⁴⁶.

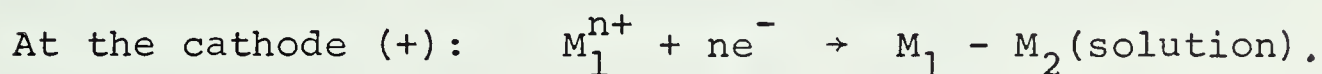
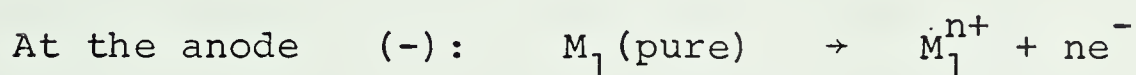
(c) M_1 exhibits no other oxidation state than n under the experimental conditions.

In addition, various experimental problems have to be solved: the measured e.m.f.'s should be ascertained as the true equilibrium e.m.f.'s; there should be no

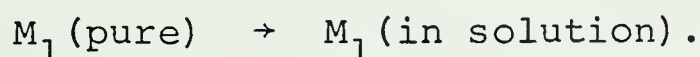
temperature gradient in the cell and no thermocouple e.m.f.'s in the electrodes; the electrolyte should be adequately purified and protected from contamination.

These conditions shall be assumed to be met in all the considerations which follow.

The electrode processes are:



The spontaneous overall cell reaction is, therefore:



The free energy change for this reaction is: $\Delta G = \mu_1 - \mu_1^\circ$, where μ_1 is the chemical potential of M_1 in solution and μ_1° its chemical potential in the pure state under experimental conditions. If this is chosen as reference state, one has: $\mu_1 = \mu_1^\circ + RT \ln a_1$, where a_1 is the activity of M_1 in solution. Hence: $\Delta G = RT \ln a_1$. The cell e.m.f. E being, at constant pressure and temperature, related to ΔG by the equation: $E = -\Delta G/nF$, one obtains finally:

$$E = -(RT/nF) \ln a_1. \quad (1)$$

Since $\mu_1 - \mu_1^\circ = g_1^m$, partial molal free energy of mixing of M_1 (1) can also be written as

$$g_1^m = nFE \quad (2)$$

The partial molal entropy of mixing of M_1 , s_1^m , is also

directly related to experimental data by:

$$s_1^m = nF dE/dT. \quad (3)$$

The partial molal enthalpy of mixing of M_1 , h_1^m , is related to the e.m.f. by the Helmholtz equation:

$$h_1^m = nF(E - TdE/dT). \quad (4)$$

It is equivalent to calculate it from: $h_1^m = g_1^m + Ts_1^m$, or, as is done in the experimental part of this work, to obtain it by extrapolating g_1^m to 0°K.

I-3. Derivation of all thermodynamic properties of a binary alloy from e.m.f. measurements

First of all some basic thermodynamic concepts concerning solutions will be recalled. Consider a thermodynamic function Z which has extensive properties, such as V (volume), U (energy), H (enthalpy), S (entropy), $F = U - TS$, $G = H - TS$, where T is the absolute temperature. Any state of the system is a function of T , the pressure P and the number of moles of the c components $n_1, n_2 \dots n_i \dots n_c$, so that:

$$dz = \left(\frac{\partial Z}{\partial T}\right)_{P, n_i} dT + \left(\frac{\partial Z}{\partial P}\right)_{T, n_i} dP + \sum_{i=1}^c \left(\frac{\partial Z}{\partial n_i}\right)_{T, P, n_j (j \neq i)} dn_i. \quad (5)$$

The partial molal property z_i for the i^{th} component is,

by definition:

$$z_i = \left(\frac{\partial Z}{\partial n_i} \right)_{T,P,n_j (j \neq i)}. \quad (6)$$

Unless otherwise specified, T and P will not be regarded as variables in what follows. To say that Z has extensive properties is to say that, whatever λ :

$$Z(\lambda n_1, \dots, \lambda n_i, \dots, \lambda n_c) = \lambda Z(n_1, \dots, n_i, \dots, n_c).$$

Hence Z is a homogeneous function of degree 1, so that, from the Euler theorem and (6):

$$Z = \sum_{i=1}^c n_i z_i. \quad (7)$$

The integral molal property z of the system is defined as: $z = Z / \sum_{i=1}^c n_i = \sum_{i=1}^c x_i z_i$, where $x_i = n_i / \sum_{i=1}^c n_i$ is

the mole fraction of the i^{th} component. It is to be noticed that, from its definition, z_i is a homogeneous function of degree 0 of the n_i (or has intensive properties), whereby it is a function of $c-1$ independent variables having the dimensions of mole ratios. This will be important in the discussion of multicomponent systems.

The change of mixing of the property Z is defined as: $Z^m = Z - \sum_{i=1}^c n_i z_i^\circ$, where the $^\circ$ superscript denotes a reference state, generally the pure state of the component under experimental conditions. It has

extensive properties, so that one can define integral and partial properties of mixing. The same is true of an excess property Z^e , defined as the difference between the actual Z and the value that it would have in an ideal solution, the latter being such that:

$\mu_i = \mu_i^o + RT \ln x_i$. The e.m.f. measurements discussed here give g_1^m , s_1^m and h_1^m (equations (2), (3), (4)).

Equation (1) and (2) are equivalent, because:

$$g_i^m = RT \ln a_i . \quad (8)$$

The latter equation defines the activity a_i of the i^{th} component in solution, with respect to a reference state. The Gibbs-Duhem equation will give the partial molal properties of M_2 from the partial molal properties of M_1 , which is enough for a complete knowledge of the thermodynamic properties of the system. This equation, obtained by differentiating (7) and comparing with (5) and (6), at constant T and P , assumes the form:

$$\sum_{i=1}^c x_i dz_i = 0, \text{ or, for a binary system:}$$

$$x_1(dz_1/dx_1) + (1-x_1)(dz_2/dx_1) = 0. \quad (9)$$

The integration of (9) gives for one of the partial molal properties of mixing obtained from e.m.f. measurements:

$$z_2^m = - \int_0^{x_1} [x_1/(1-x_1)] dz_1^m \quad . \quad (10)$$

Equation (10) can be modified if z is the free energy, owing to (8), giving:

$$\log a_2 = - \int_0^{x_1} [x_1/(1-x_1)] d(\log a_1) \quad , \quad (11)$$

or, using the activity coefficients $\gamma_1 = a_1/x_1$ and $\gamma_2 = a_2/x_2$:

$$\log \gamma_2 = - \int_0^{x_1} [x_1/(1-x_1)] d(\log \gamma_1) \quad . \quad (12)$$

Equations (11) and (12) are valid if M_2 in its pure state is chosen as reference for activities. The form (12) is the most convenient, since both $x_1/(1-x_1)$ and $\log \gamma_1$ remain finite except for $x_1 = 1$. It can be shown that for this limit, the integral is converging, since it can be rewritten as:

$$\begin{aligned} \log \gamma_2 = & - [x_1 x_2 \log \gamma_1 / (1-x_1)^2]_0^{x_1} \\ & + \int_0^{x_1} [\log \gamma_1 / (1-x_1)^2] dx_1 \quad . \quad (13) \end{aligned}$$

The quantity $\log \gamma_1 / (1-x_1)^2$ generally assumes a finite limit for $x_1=1$. This fact can be explained by the theory of regular solutions, due to Hildebrand²⁷. In this theory, one obtains for $\log \gamma_1$ and $\log \gamma_2$ expressions of the form: $\log \gamma_1 = (A/2.3RT)x_2^2$ and

$\log \gamma_2 = (A/2.3RT)x_1^2$. Similarly, integrals in equations (10) to (13) can be shown to converge if the lower integration limit is taken as 1, but then one has to modify these equations in order to include $z_2^m(x_1=1)$ or $\gamma_2(x_2=1)$ unless the reference state for M_2 is chosen as the infinitely dilute solution of M_2 in M_1 . Convergence requirements for the integration limit $x_1 = 1$ are found to be met for all extensive thermodynamic properties, in particular for H and S .

In conclusion, it appears that all the thermodynamic properties of the $M_1 - M_2$ alloy can, in theory, be calculated from the e.m.f. of the cell described previously. Since there is very little dependence of E upon P , these calculations are practically restricted to G , S and H .

As an example of such calculations, the work of Seltz⁴⁷ can be mentioned. This author applied various graphical methods of integration of the Gibbs-Duhem equation, using equations (11) to (13), to e.m.f. data for the zinc-antimony system.

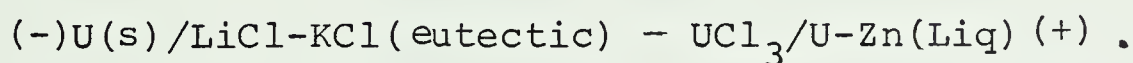
I-4. E.m.f. measurements and binary phase equilibria

In alloy systems, binary liquid-solid phase diagrams can be obtained directly from e.m.f. measurements. More general thermodynamic methods can be applied to

the correlations of the data obtained from e.m.f. measurements with the data obtained from binary phase equilibria.

I-4-1. Direct method of determination of phase diagrams

In a cell where the $M_1 - M_2$ alloy is liquid, the e.m.f. can be studied at constant temperature and variable composition. If the temperature is such that the liquidus line is met, a break and a plateau are observed as saturation is reached. Analysis of the liquid and the solid phases beyond this break will give both the liquidus and the solidus points at the temperature considered. In many cases, however, it is not possible to separate the liquid from the solid phase. The analysis of the whole mixture at the break will then give the liquidus point. For example, Hoshino and Plambeck⁴⁸ studied liquid uranium-zinc alloys from the e.m.f. of the cell:



In this case, it is not possible to analyse separately the liquid and the solid phases, but only to obtain the uranium content of the alloy at the break (Fig. 1). This was found by the authors⁴⁸ to be $x_U = 2.2 \times 10^{-2}$ mole p.c., at 808°K, falling between previous literature values. Similar investigations were made by Volkovich et al.⁴⁹, for the uranium-zinc system, and by Kober

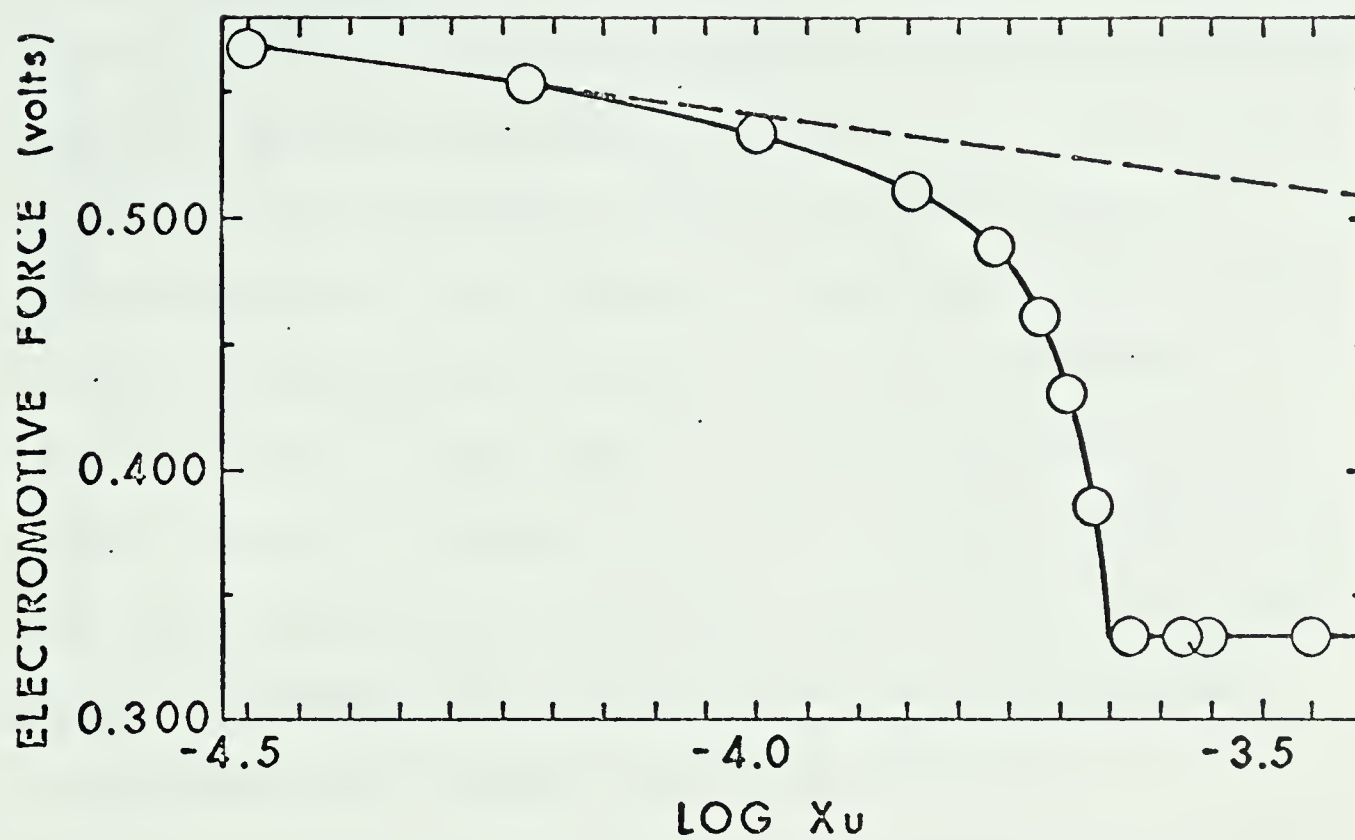


Figure 1. E.m.f. of the cell $(-)U(s)/LiCl-KCl(eut.)-UCl_3/U-Zn(+)(liq.)$ as a function of x_U , at $808^\circ K$ (from the work of Hoshino and Plambeck⁴⁸).

et al.⁵⁰, for the lanthanum-bismuth system.

If the liquidus line intercepts a constant-temperature line at several points, the e.m.f.-composition curve will show several plateaus. This has been observed⁵¹ in e.m.f. experiments on the uranium-bismuth system, the phase diagram of which is not known; these experiments established, however, the existence in this diagram of four regions of constant uranium activity, corresponding to equilibria with compounds including UBi_2 , UBi_4 , UBi . In the same manner, the e.m.f. study of Dubinin et al.⁵², giving a small part of the beryllium-zinc liquidus, which otherwise is not known, provides some evidence that no intermetallic compounds exist between beryllium and zinc.

I-4-2. Computational methods of determination of phase diagrams

I-4-2-1. Complete miscibility in both the liquid and the solid phases.

If there is complete miscibility in both the liquid and the solid phases, the phase diagram can be calculated according to the difference method proposed by Seltz^{28,29}. In this method, one plots at a constant temperature T_0 the activities of both components, M_1 and M_2 , with respect to a common standard state for each component, in the liquid and the solid phase, against the mole fraction of one of the components in the

corresponding phase (Fig. 2). If there is a liquid-solid equilibrium, one has: $a_1(l) = a_1(s)$, and $a_2(l) = a_2(s)$, where (l) and (s) refer to the liquid and the solid, respectively. In addition, the following equations can be written between the mole fractions: $x_1(l) + x_2(l) = 1$, and $x_1(s) + x_2(s) = 1$, whereby $x_1(l) - x_1(s) = x_2(l) - x_2(s)$, or, if: $\Delta x_1 = x_1(l) - x_1(s)$ and: $\Delta x_2 = x_2(l) - x_2(s)$, $\Delta x_1 = \Delta x_2$. The curves obtained by plotting Δx_1 and Δx_2 at constant activity of M_1 and M_2 , respectively, will intercept at point I (Fig. 2), if the liquidus or the solidus lines are encountered at T_0 . The abscissa of I gives one point of the liquidus (Fig. 2). The corresponding point of the solidus is obtained by taking the abscissa of point C_1 or C_2 , where the activity is the same as in B_1 or B_2 , which are the intercepts of a vertical line going through I, with the $a_1(l)$ and $a_2(l)$ curves, respectively (Fig. 2). From this construction, two points $P(l)$ and $P(s)$ of the diagram are obtained (Fig. 2). If the temperature is such that neither the liquidus nor the solidus lines will be encountered, the Δx_1 and Δx_2 curves will not intercept. They can also intercept at two points, if the phase diagram shows a minimum.

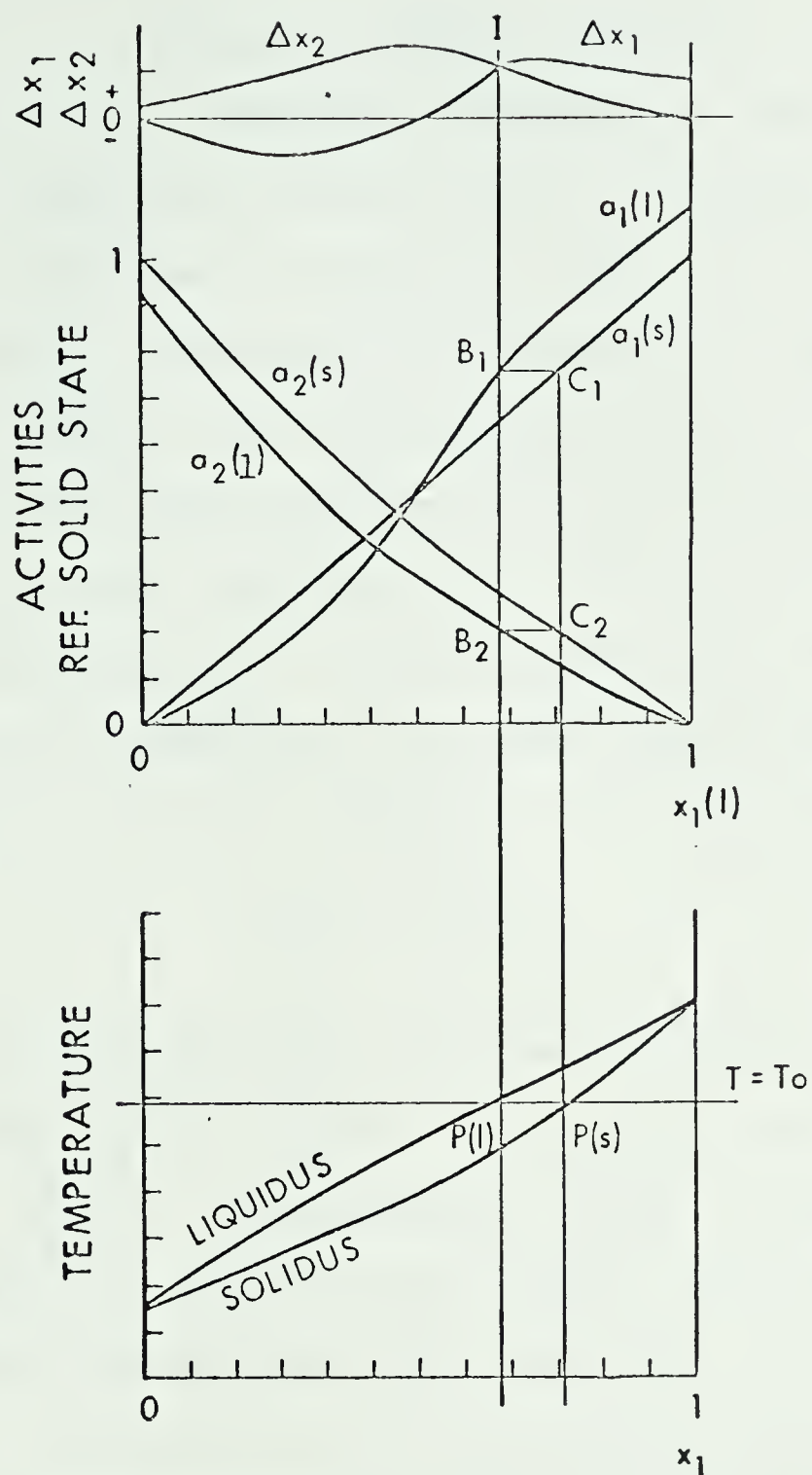


Figure 2. Application of the method of Seltz^{28,29} to the computation of a phase diagram from activity data (complete miscibility in both the solid and the liquid phase).

I-4-2-2. Simple eutectic

If there is complete miscibility in the liquid phase, but no significant miscibility in the solid phase, a eutectic point may be observed (Fig. 3). The previous method is no longer applicable and can be replaced by another method, due to Dunkerley and Mills²³. If $x_1(e)$ is the mole fraction of M_1 in the eutectic, for $x_1 > x_1(e)$, the liquid solution will be in equilibrium with pure solid M_1 . On the liquidus line, the activity of M_1 , with reference to the pure liquid state will be the same in both the liquid and the solid phases:

$$a_1(l) = a_1(s) .$$

$a_1(l)$ is obtained from e.m.f. measurements. $a_1(s)$ is such that: $\mu_1^\circ(s) = \mu_1^\circ(l) + RT \ln a_1(s)$, or: $RT \ln a_1(s) = \mu_1^\circ(s) - \mu_1^\circ(l)$. The quantity: $-(\mu_1^\circ(s) - \mu_1^\circ(l))$ is the free energy of fusion of M_1 , easily obtained from standard thermodynamic data. The plot of:

$(\mu_1^\circ(l) - \mu_1^\circ(s))/T$ vs. $1/T$ is a straight line (Fig. 3).

Its intercepts with the plots of: $R \ln a_1(l)$ vs $1/T$ which are also straight lines, gives points of the liquidus.

For example (Fig. 3), the $R \ln a_1$ vs. $1/T$ line for $x_1 = x_{10}$ intercepts the $(\mu_1^\circ(s) - \mu_1^\circ(l))/T$ vs. $1/T$ line for: $1/T = 1/T_0$; hence the point (x_{10}, T_0) of the liquidus.

For $x_1 < x_1(e)$, the liquid is in equilibrium with M_2 ;

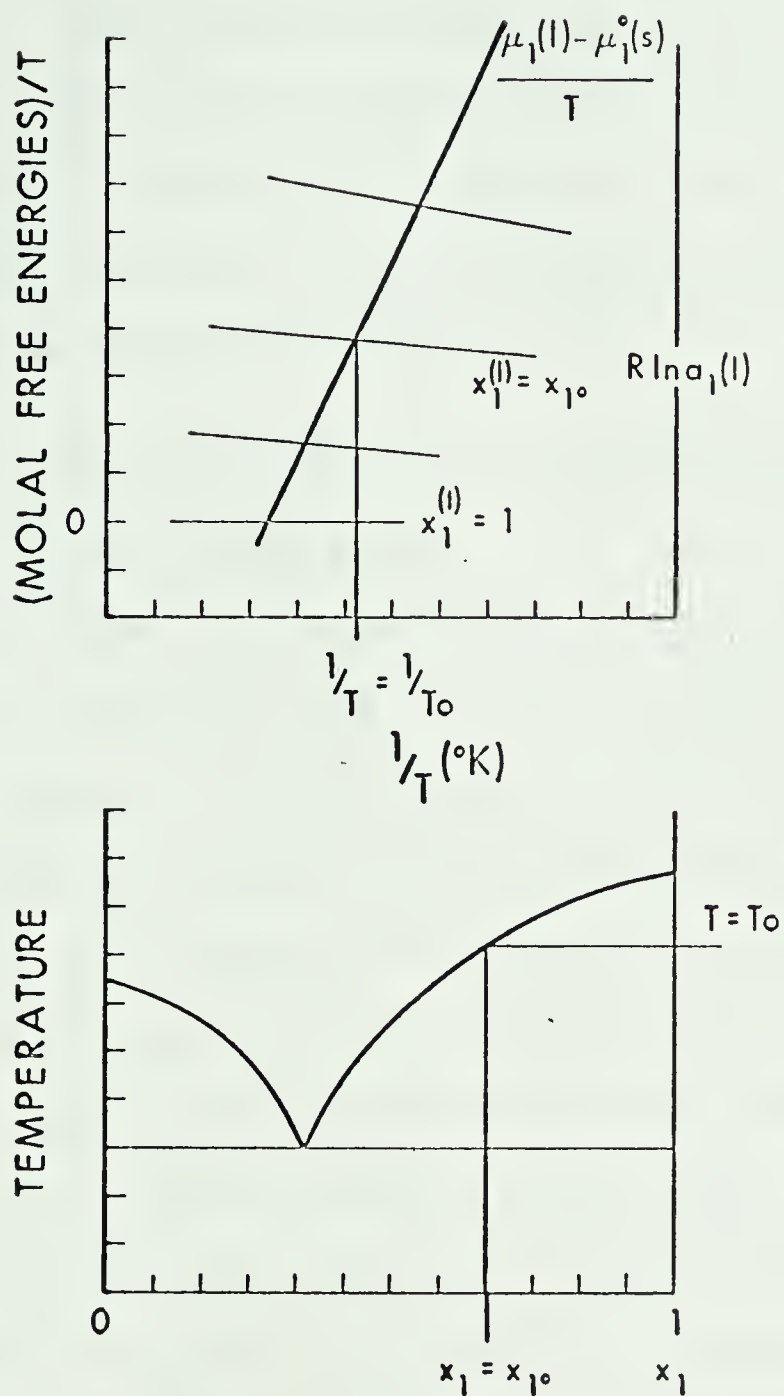


Figure 3. Application of the method of Dunkerley and Mills²³ to the computation of a phase diagram from activity data (simple eutectic).

$a_2(l)$ is obtained by integration of the Gibbs-Duhem equation. This method was applied to the zinc-tin system, where no appreciable solid solubility exists ²⁴, by Dunkerley and Mills ²³. The computed phase diagram is in good agreement with the diagrams previously obtained by thermal analysis ⁵³⁻⁵⁵.

I-4-2-3. Eutectic with partial miscibility in the solid phase

Where there is a eutectic with a significant range of solid solubility (Fig. 4), e.m.f. measurements can also be applied. For example, the tin-bismuth phase diagram was studied by Seltz and Dunkerley ^{23,56}. In this work, the authors establish the β -solidus compositions by writing, as in the previous case, that: $a_{\text{Sn}}(l) = a_{\text{Sn}}(s)$, both activities being taken with respect to a common standard state, such as liquid tin. Assuming ideal behaviour of the β -solid solution, one obtains: $x_{\text{Sn}}(s) = a_{\text{Sn}}(l)/a_{\text{Sn}}^{\circ}(s)$, where $a_{\text{Sn}}^{\circ}(s)$ is the activity of pure solid tin. Accepting the published β -liquidus ^{57,58}, $a_{\text{Sn}}(l)$ being obtained from e.m.f. measurements and $a_{\text{Sn}}^{\circ}(s)$ from standard thermodynamic data, one can calculate from this relationship the β -solidus. The α -solidus was similarly calculated by the authors, and the α -liquidus was corrected to satisfy the above equation.

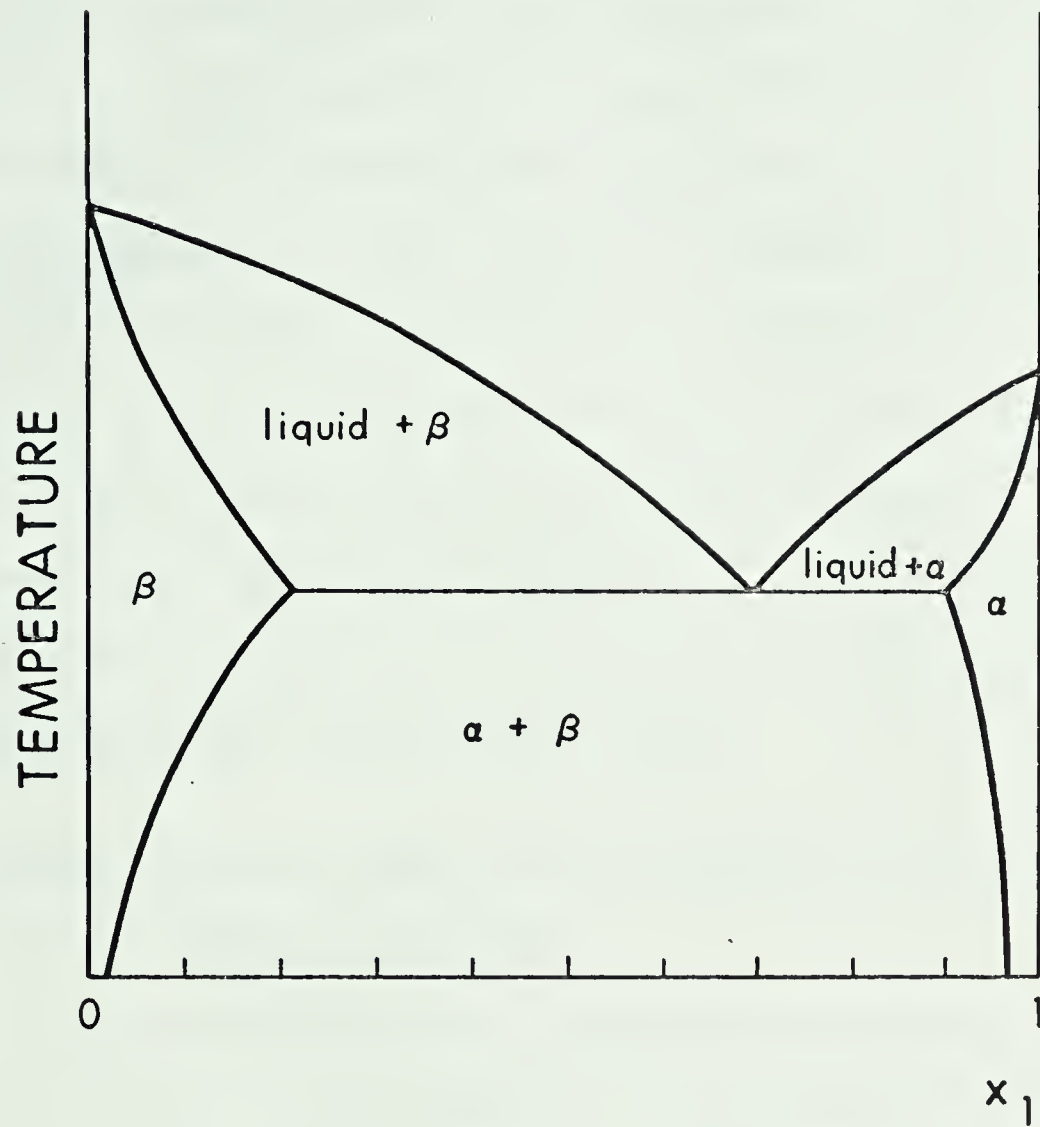


Figure 4. Phase diagram showing a eutectic with solid solubility.

I-4-2-4. Other cases

Thermodynamic calculations from e.m.f. measurements also have ascertained the existence of a peritectic point in the lead-bismuth system ^{23,59,60}. Dunkerley and Mills ²³ discussed the applications of e.m.f. measurements to other types of diagrams, such as diagrams including a monotectic, a eutectoid or a peritectoid. As an example of calculation of such a diagram, one can mention the e.m.f. works of Kleppa ⁶¹ and Rosenthal, Mills and Dunkerley ⁶², who calculated the monotectic point and the liquidus in the lead-zinc diagram which are reviewed below.

I-4-3. Other types of correlation of e.m.f. data with phase equilibria

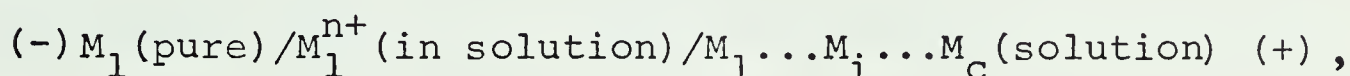
The calculation of a liquid-solid phase diagram from e.m.f. data is an example of direct correlation of the e.m.f. data with thermal analysis data concerning this phase diagram. Lumsden ⁶³ gives more elaborate examples of such correlations, involving either the liquid-solid equilibria or the liquid-vapour equilibria (vapour pressure measurements).

White et al. ⁶⁴ correlate e.m.f. data, vapour pressure data and calorimetric data in the silver-gold system.

I-5. E.m.f. measurements and multicomponent alloys

I-5-1. General considerations

So far only binary alloys have been considered, but it is obvious that the e.m.f. methods of investigation can be extended to multicomponent alloys by using cells such as:



where c is the number of components. The conditions that have to be fulfilled by the system and with respect to experimental conditions are the same as for binary systems. Equations (1) to (4) are still valid, but the integration of the Gibbs-Duhem equation in binary systems is no longer valid. A more general theory will be derived here.

I-5-2. Calculation of an integral molal property from a partial molal property

Darken³¹ found a method whereby values for an integral molal property of a system can be computed from values for one partial molal property. Balesdent³³ formulated the theory of Darken in a somewhat more general manner. This formulation will be used here.

Consider an integral molal property z and a corresponding partial molal property z_i . What is sought is a relationship between z and z_i . Let $z(x_1\dots x_i\dots x_c)$ be

an analytical expression of z . This gives, by differentiating: $dz = \sum_{i=1}^c \left(\frac{\partial z}{\partial x_i} \right) dx_i$; the partial derivatives bear no subscripts because they are purely mathematical symbols: because of the relation: $\sum_{i=1}^c x_i = 1$, it is not possible, while x_i is varying, to keep all the other variables at an arbitrary constant value, so that the expression: $\left(\frac{\partial z}{\partial x_i} \right)_{x_j (j \neq i)}$, where the subscript means that the derivation is made at constant x_j , for $j \neq i$, has no physical meaning whatsoever. Another expression of dz , obtained by differentiating: $z = \sum_{i=1}^c x_i z_i$ gives, taking into account the Gibbs-Duhem equation: $dz = \sum_{i=1}^c z_i dx_i$. The constraint: $f(x_1 \dots x_i \dots x_c) = \sum_{i=1}^c x_i - 1 = 0$ being imposed on the system, the problem can be solved by a method similar to the method of Lagrange multipliers. α being the multiplier:

$$\sum_{i=1}^c \left(\frac{\partial z}{\partial x_i} - z_i - \alpha \frac{\partial f}{\partial x_i} \right) dx_i = 0. \quad (14)$$

In order that the term in dx_1 vanish, one must have (taking into account $\frac{\partial f}{\partial x_i} = 1$): $\frac{\partial z}{\partial x_1} - z_1 - \alpha = 0$. If α is chosen to satisfy the latter equation, the $c-1$ remaining dx_i are now independent, so that (14) is identically zero, whereby: $\frac{\partial z}{\partial x_i} - z_i - \alpha = 0$, or:

$$z_i = \frac{\partial z}{\partial x_i} - \alpha, \quad (15)$$

which is valid for all i 's since it is valid for $i=1$.

Substituting z_i from (15) in: $z = \sum_{i=1}^c x_i z_i$, one gets:

$$\alpha = -z + \sum_{i=1}^c x_i \frac{\partial z}{\partial x_i}, \text{ so that (16) gives, for } i=1:$$

$$z_1 = z + (1-x_1) \frac{\partial z}{\partial x_1} - \sum_{i=2}^c x_i \frac{\partial z}{\partial x_i}. \quad (16)$$

Equation (16) is applicable when an analytical expression of z is known. Let this be illustrated by two examples.

Example 1: A regular binary solution is defined by:

$h^e = Ax_1x_2$, the entropy being the same as in ideal solutions, so that $s^e = 0$. Then: $g^e = Ax_1x_2$, whence, applying (16): $g_1^e = g^e + (dg^e/dx_1)(1-x_1) - x_2(dg^e/dx_2)$.

This gives: $g_1^e = Ax_2^2$ and, similarly: $g_2^e = Ax_1^2$, or, in terms of activity coefficients: $\log \gamma_1 = (A/2.3RT)x_2^2$, and: $\log \gamma_2 = (A/2.3RT)x_1^2$. These expressions are identical to those mentioned above (I-3).

Example 2: In their work on the silver-gold system ⁶⁴, White et al. obtain for the g^e of the liquid solution:

$$g^e = -(4656 - 800 x_{Au} - 1.375T)x_{Au}(1-x_{Au}).$$

The application of (16) to this expression gives:

$$g_{Ag}^e = -(5456 - 1600 x_{Au} - 1.375T)x_{Au}^2$$

and

$$g_{Au}^e = -(4656 - 1600 x_{Au} - 1.375T)x_{Ag}^2.$$

These equations are identical to the equations obtained

by the authors by integration of the Gibbs-Duhem equation, the form of which is identical to (16) in binary systems.

Equation (16) can be modified to obtain an expression more suitable for calculations from experimental data. For this purpose, $c-1$ independent variables $\lambda_1 \dots \lambda_i \dots \lambda_{c-1}$ must be chosen, whereby (16) becomes:

$$z_1 = z - (1-x_1) \sum_{i=1}^c \left(\frac{\partial z}{\partial \lambda_i} \right)_{\lambda_j} \frac{\partial \lambda_i}{\partial x_1} - \sum_{i=1}^c \left(\frac{\partial z}{\partial \lambda_i} \right)_{\lambda_j} \sum_{k=2}^c x_k \frac{\partial \lambda_i}{\partial x_k} \quad (j \neq i)$$

If the λ_i are so chosen that (taking into consideration: $\sum_{i=1}^c x_i = 1$):

$$\sum_{k=1}^c x_k \frac{\partial \lambda_i}{\partial x_k} = 0, \quad (17)$$

for $i \geq 2$, and $\lambda_1 = x_1$, equation (16) takes the form:

$$z_1 = z + (1-x_1) \left(\frac{\partial z}{\partial x_i} \right)_{\lambda_i} \lambda_i \quad (i \geq 2) \quad (18)$$

Previous authors^{31, 33} have chosen, in accordance with (18): $\lambda_i = x_i/x_c$ for $i \geq 2$. The one-dimensional part of the phase diagram obtained by keeping the (x_i/x_c) 's constant is called a pseudo-binary line, since (18) is similar to the classical equation:

$$z_1 = z + (1-x_1) (dz/dx_1) \quad (19)$$

obtained in binary systems from the Gibbs-Duhem equation.

In the triangular representation of a ternary diagram, pseudo-binary lines are straight lines passing through one corner (Fig. 5). It is to be noticed that equation (18) is not only valid for the set of variables which has just been introduced since it is valid for any set of λ_i 's ($i \geq 2$) that will satisfy (17), with $\sum_{i=1}^c x_i = 1$. It is easy to see that the acceptable forms of the λ_i 's will be functions of the (x_i/x_c) 's, hence the importance of pseudo-binary systems in this theory.

In measurements such as e.m.f. measurements, z_1 is known and z unknown, so that one has to integrate (18).

This gives:

$$z/(1-x_1) = \left[\lim_{x_1 \rightarrow a} [z/(1-x_1)] + \int_a^{x_1} [z_1/(1-x_1)^2] dx_1 \right]. \quad \lambda_i (i \geq 2) \quad (20)$$

The subscript λ_i indicates that the limit and the integral are calculated with the λ_i 's ($i \geq 2$) kept constant. This is of practical interest only if: $L = \lim_{x_1 \rightarrow a} [z/(1-x_1)]$ is

obtainable. In general (as discussed by Vaisburd et al.³⁴), the value $z(a)$ of z for $x=a$ must be known and L is finite. If $a=0$, this value is derived from the study of the $(c-1)$ -component system $M_2 \dots M_c$ ³¹. Therefore, for $a < 1$:

$$z = (1-x_1) [z(a)/(1-a)] + \int_0^a [z_1/(1-x_1)^2] dx_1. \quad \lambda_i (i \geq 2) \quad (21)$$

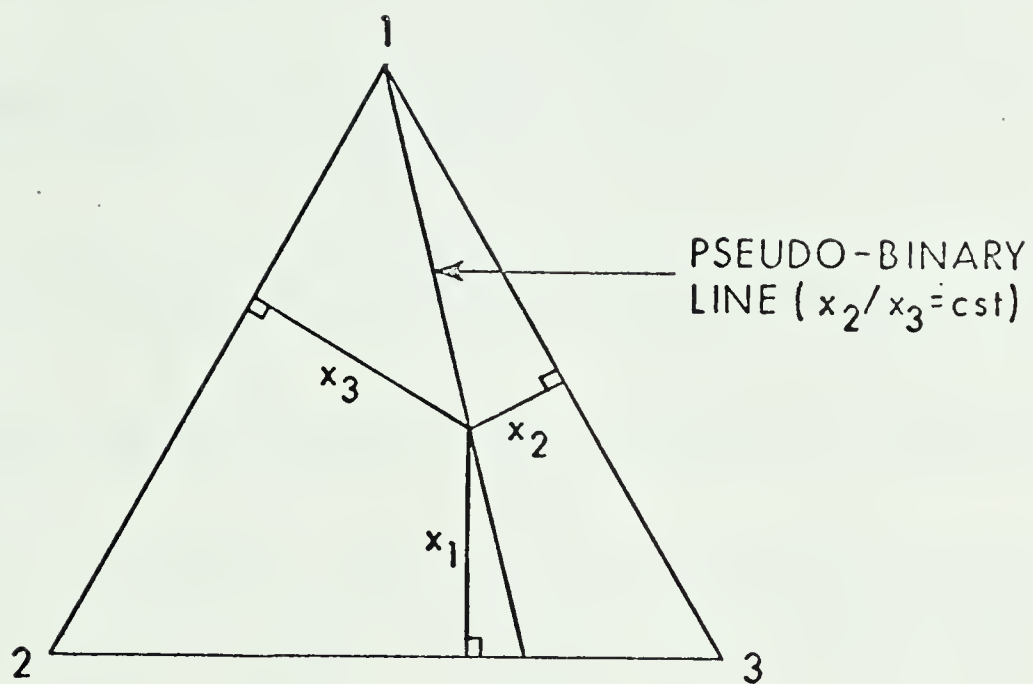


Figure 5. Representation of compositions in triangular coordinates for a ternary system, showing a pseudo-binary line.

For $a=1$, (21) is no longer valid but an equation can be derived if z is a property of excess z^e . According to the de l'Hopital theorem: $L = \lim_{x_1 \rightarrow 1} \left(\frac{\partial z^e}{\partial x_1} \right)_{\lambda_i (i \geq 2)}$ whence,

$$\text{applying (18): } L = -\lim_{x_1 \rightarrow 1} [(z_1^e - z^e)/(1-x_1)].$$

Since: $z^e = \sum_{i=1}^c x_i z_i^e$ and $x_i = (1-x_1)/(1 + \sum_{j \neq 1, i} x_j/x_i)$, one has

$$L = \lim_{x_1 \rightarrow 1} [-z_1^e + \sum_{i=2}^c [z_1^e/(1 + \sum_{j \neq 1, i} x_j/x_i)]]]. \text{ The limit being}$$

taken at constant λ_i 's, i.e. at constant (x_i/x_c) 's, the terms $x_j/x_i = (x_j/x_c) \cdot (x_c/x_i)$ are constant and:

$$L = (-z_1^e)_{x_1=1} + \sum_{i=2}^c [1/(1 + \sum_{j \neq 1, i} x_j/x_i)] (z_i^e)_{x_1=1}. \text{ If the}$$

standard state is so chosen that for each component $z_i^e = 0$, (i.e. pure state for M_1 and infinitely dilute state in M_1 solution for the others) (20) becomes:

$$z^e = (1-x_1) \left[\int_1^{x_1} [z_1^e/(1-x_1)^2] dx_1 \right]_{\lambda_i (i \geq 2)}. \quad (22)$$

If, however, the standard state is chosen as the pure state for all components, then (20) becomes:

$$z^e = (1-x_1) \left[\int_1^{x_1} [z_1^e/(1-x_1)^2] dx_1 \right]_{\lambda_i (i \geq 2)} + \sum_{i=2}^c x_i (z_i^e)_{x_1=1}.$$

$(z_i^e)_{x_1=1}$ can be calculated by integration of (19) on the

$M_1 - M_i$ binary line, which gives:

$$(z_i^e)_{x_1=0} = 0 = \lim_{x_1 \rightarrow 1} [z^e/(1-x_1)] + \int_1^0 [z_1^e/(1-x_1)^2] dx_1.$$

On noting that: $z^e = x_1 z_1^e + (1-x_1) z_i^e$, this gives

$$(z_i^e)_{x_1=1} = -\lim_{x_1 \rightarrow 1} [z_1^e/(1-x_1)] - \int_1^0 [z_1^e/(1-x_1)^2] dx_1.$$

Assuming that z_1^e is proportional to $(1-x_1)^2$ in the vicinity of $x_1=1$, (regular behaviour for $z=g$) which is generally true³¹, one can see that the above limit is zero, whereby:

$$z^e = (1-x_1) \left[\int_1^{x_1} [z_1^e/(1-x_1)^2] dx_1 \right]_{\lambda_i (i \geq 2)} + \sum_{i=2}^c \left[\int_0^1 [z_1^e/(1-x_1)^2] dx_1 \right]_{M_1-M_i \text{ binary}} \quad (23)$$

The subscript " M_1-M_i binary" indicates that the integration is carried out on the M_1-M_i binary line.

Once z is known from z_1 , or z^e from z_1^e , one can obtain all the other partial molal properties by using (18).

Elliott and Chipman^{23,35,36, 65}, Mellgren⁶⁶, and other authors³⁷⁻³⁹ have applied the method of Darken to several ternary intermetallic systems studied by e.m.f. methods.

I-5-3. Calculation of a partial molal property
from another partial molal property

As has just been discussed, Darken³¹ indirectly solved this problem. Other authors^{32,67-71} attempted to solve it directly. This subject has been reviewed^{72,73}.

Since $dz = \sum_{i=1}^c z_i dn_i$ is a complete differential, one has:

$$\left(\frac{\partial z_2}{\partial n_1}\right)_{n_2} = \left(\frac{\partial z_1}{\partial n_2}\right)_{n_1}, \quad (24)$$

the subscript n_1 indicating that the derivative is taken at n_1 and all the other variables but n_2 constant, and the subscript n_2 having a similar meaning. This is one of the basic relationships between two partial molal properties. From an experimental point of view, however, the absolute numbers of moles are not practical variables.

Following the method used above, one can first use the x_i as variables on a purely analytical basis. This change of variables gives:

$$\frac{\partial z_2}{\partial x_1} - \sum_{i=1}^c x_i \frac{\partial z_2}{\partial x_i} = \frac{\partial z_1}{\partial x_2} - \sum_{i=1}^c x_i \frac{\partial z_1}{\partial x_i}. \quad (25)$$

Using $\lambda_1 \dots \lambda_{c-1}$ as the $c-1$ independent variables for practical calculations, one can see that, choosing $\lambda_i (i \geq 3)$ as a homogeneous function of zeroth degree of $c-1$ of the x_i 's, and independent of x_1 and x_2

(practically this will be restricted to $\lambda_i = x_i/x_c$ for $i \geq 3$), and λ_2 such that: $\frac{\partial \lambda_2}{\partial x_1} = \sum_{i=1}^c x_i \frac{\partial \lambda_2}{\partial x_i}$, so that

the term in $(\frac{\partial z_2}{\partial \lambda_2} \lambda_1)$ will vanish and integration will

be possible:

$$\left(\frac{\partial z_2}{\partial \lambda_1 \lambda_2}\right) \left[\frac{\partial \lambda_1}{\partial x_1} - \sum_{i=1}^c x_i \frac{\partial \lambda_1}{\partial x_i}\right] = \sum_{i=1}^2 \left[\frac{\partial z_1}{\partial \lambda_i} \left(\frac{\partial \lambda_i}{\partial x_2} - \sum_{k=1}^c x_k \frac{\partial \lambda_i}{\partial x_k}\right)\right]. \quad (26)$$

All the variables discussed below shall conform to the above conditions, so that (26) will be applicable to

them. Gokcen³² has chosen: $\lambda_1 = x_c/(1-x_2)$ and $\lambda_2 = x_c/(1-x_1)$, which gives, from (26): $\left(\frac{\partial z_2}{\partial \lambda_1 \lambda_2}\right) \left(\frac{\partial \lambda_1}{\partial x_2}\right) =$

$\left(\frac{\partial z_1}{\partial \lambda_2 \lambda_1}\right) \left(\frac{\partial \lambda_2}{\partial x_1}\right)$ and integrating:

$$z_2(\lambda_1, \lambda_2) = z_2(0, \lambda_2) + \int_0^{\lambda_1} (\lambda_2/\lambda_1)^2 \left(\frac{\partial z_1}{\partial \lambda_2 \lambda_1}\right) d\lambda_1. \quad (27)$$

The set of variables $\lambda_i = x_i/x_c$, for all i's gives similar results.

In the theory of Wagner⁶⁷, generalized by Gokcen³²,

the variables were: $\lambda_1 = x_1$, $\lambda_2 = [1-(x_1+x_2)]/(1-x_1)$ and

$\lambda_i = (x_i/x_c)$ for $i \geq 3$. Then (26) gives:

$$\left(\frac{\partial z_2}{\partial x_1}\right)_{\lambda_2} = [\lambda_2/(1-x_1)^2] \left(\frac{\partial z_1}{\partial \lambda_2}\right)_{x_1} - [x_1/(1-x_1)] \left(\frac{\partial z_1}{\partial x_1}\right)_{\lambda_2}.$$

Upon integration, one obtains a general form of the equation of Wagner ⁶⁷:

$$\begin{aligned} z_2(x_1, \lambda_2) = & z_2(a, \lambda_2) + \int_a^{x_1} [z_1/(1-x_1)^2] dx_1 \\ & - \int_a^{x_1} \lambda_2 \frac{\partial}{\partial \lambda_2} [z_1/(1-x_1)^2]_{x_1} dx_1 - [x_1/(1-x_1)] z_1(x_1, \lambda_2) \Big|_a^{x_1}, \end{aligned} \quad (28)$$

the integration being carried out at constant λ_2 , x_i/x_c ($i \geq 3$). If the lower integration limit is chosen as $a=1$, one obtains, for a property of excess, by the method already used for (22) and (23), the pure states being taken as references for all components:

$$\begin{aligned} z_2^e(x_1, \lambda_2) = & \left[\int_0^1 [z_1^e/(1-x_1)^2] dx_1 \right]_{M_1-M_2 \text{ binary}} + \int_1^{x_1} [z_1^e/(1-x_1)^2] dx_1 \\ & - \int_1^{x_1} \lambda_2 \frac{\partial}{\partial \lambda_2} [z_1^e/(1-x_1)^2]_{x_1} dx_1 - [x_1/(1-x_1)] z_1^e(x_1, \lambda_2), \end{aligned} \quad (29)$$

the integration being carried out at constant λ_2 , x_i/x_c ($i \geq 3$) except for the term bearing the subscript " M_1-M_2 binary". The limit of $z_1/(1-x_1)^2$ is assumed

to be finite when $x_1 \rightarrow 1$.

Blander and Hagemark⁷¹ used the same variables as Wagner⁶⁷; the final formulae obtained by these authors for ternary systems are reported by Guion⁷³.

The set of variables $\lambda_1 = x_1$, $\lambda_i = x_i/x_c$ for $i \geq 2$, gives equations very similar to (28) and (29).

Another set of variables that has interesting properties consists of $\lambda_1 = z_1$, $\lambda_2 = x_2/x_c \dots \lambda_{c-1} = x_{c-1}/x_c$. Since z_1 is generally not known analytically, but from experimental points, it is best to start from:

$\left(\frac{\partial z_2}{\partial \lambda_1}\right)_{\lambda_2} = \left(\frac{\partial z_1}{\partial \lambda_2}\right)_{\lambda_1}$, obtained with $\lambda_i = x_i/x_c$ for all i 's, and not from (27). This gives: $\left(\frac{\partial z_2}{\partial z_1}\right)_{\lambda_2} \left(\frac{\partial z_1}{\partial \lambda_1}\right)_{\lambda_2} = \left(\frac{\partial z_1}{\partial \lambda_2}\right)_{\lambda_1}$, or:

$$\left(\frac{\partial z_2}{\partial z_1}\right)_{\lambda_2} = \left(\frac{\partial z_1}{\partial \lambda_2}\right)_{\lambda_1} \bigg/ \left(\frac{\partial z_1}{\partial \lambda_1}\right)_{\lambda_2}, \text{ and, regarding } \lambda_1 \text{ as an}$$

implicit function of λ_2 :

$$\left(\frac{\partial z_2}{\partial z_1}\right)_{\lambda_2} = - \left(\frac{\partial \lambda_1}{\partial \lambda_2}\right)_{z_1}. \quad (30)$$

McKay^{68,69} and Schuhmann⁷⁰ carried out directly the integration of (30), which gives:

$$z_2(b, \lambda_2 \dots \lambda_{c-1}) = z_2(a, \lambda_2 \dots \lambda_{c-1}) - \int_a^b \left(\frac{\partial \lambda_1}{\partial \lambda_2}\right)_{z_1} dz_1, \quad (31)$$

where a and b represent two values of z_1 . The function being integrated can be obtained, in ternary systems, by a geometric construction⁷⁰ using the constant z_1 curves

in triangular coordinates. The authors⁶⁸⁻⁷⁰ actually started, not from (30) but from: $\left(\frac{\partial z_2}{\partial z_1}\right)_{n_2} = -\left(\frac{\partial n_1}{\partial n_2}\right)_{z_1}$, a straightforward consequence of (24). Gokcen³² obtains from (30) not only (31) but also (28) and (29).

Experimental applications of this theory can be found in the articles quoted here^{32,67-71,73}. Mostly ternary metal systems have been investigated, in many cases by e.m.f. methods. The work of Guion⁷³ is mentioned here, although the system investigated was not a metallic solution, but a ternary molten salt mixture: the experimental e.m.f. methods used are, in this work, very close to those used in metal systems.

I-5-4. Conclusion on multicomponent systems

The theory of Darken³¹, concerning the relationship between z and z_1 , was derived according to a method due to Balesdent³³. The basic assumptions of the theory are: (a) the extensive properties of Z and: (b) that Z is a well-behaved function of c variables at constant T and P . From these assumptions, equation (16) was derived, using the x_i as variables. This equation is of purely analytical interest, due to the constraint: $\sum_{i=1}^c x_i = 1$. Equation (18) was then derived with satisfactory independent variables, and integrated, leading to (21), (22), and (23). This method is extended here to the relationship between z_1 and z_2 . From the same assumptions,

(25), an analytical equation, and (26), using adequate independent variables, were derived. Equations previously reported ^{32, 67-71} were found to derive from (25) or (26) by an appropriate choice of the independent variables. Some other choices have been proposed as examples.

This is a purely thermodynamic theory, in that it does not assume anything about the form of $z(x_1 \dots x_c)$ or $z_1(x_1 \dots x_c)$. This form is what is obtained in (for example) e.m.f. experiments.

Various authors, however, discussed models for metallic solutions ⁷⁴⁻⁸⁰. The regular model, mentioned here for binary solutions, has been widely used. Except in a few cases ⁶⁴, the results are satisfactory only in the low concentration range. Olson and Toop ⁷⁵, having calculated the excess molal free energy in the Sb-Cd-Pb and Bi-Cd-Sn systems, from a regular model, compared their results with calculations from experimental e.m.f. data by the method of Darken ^{35,36,65,66}. The results showed that the model is only a first approximation, useful to estimate data where no literature is available.

I-6. Specific case of the lanthanum zinc system

In the experimental part of this work, liquid lanthanum-zinc alloys have been studied by e.m.f. methods. This investigation has been made in connection with

electrochemical processes for separation of fission impurities from uranium in liquid metal solutions.

In some methods of processing spent nuclear reactor fuels, the fuel is first dissolved in liquid zinc or liquid bismuth⁸¹⁻⁸⁴. Numerous studies involving solutions of uranium in liquid metals have been made. Investigations concerning the separation of fission products by oxidation-reduction reactions have been conducted⁸⁵⁻⁸⁷. The diffusivity of uranium in liquid metal solutions has been measured⁸⁸. Studies of dilute metallic solutions of uranium have been made by electromotive force methods, both in zinc^{48,49,89} and in bismuth⁹⁰. Solubility data for various metals in liquid zinc have been compiled by Johnson and Dillon⁹¹.

It is well known that the fission of uranium-235 gives primarily one fragment of about 90 - 100 a.m.u. and another of about 135 - 145 a.m.u. In the first group, one finds nine isotopes of yttrium. In the second group, one finds seven isotopes of lanthanum, together with isotopes of cerium, praseodymium, neodymium and other rare earth metals^{92,93}. Furthermore, stable isotopes such as Y-89, La-139, Ce-140 are the terminal products of decomposition of short-lived fission impurities^{92,93}. It is therefore desirable to study

solutions of rare earth metals in liquid metals, as they are typical fission impurities. The yttrium-zinc system has been studied by Chiotti et al.⁹⁴ from vapour pressure measurements; the e.m.f. study of Hoshino and Plambeck⁹⁵ on this system has not yet been published. E.m.f. experiments on the lanthanum-bismuth system⁵⁰, on solutions of cerium and erbium in molten zinc, lead, cadmium and bismuth⁹⁶ have been made. In this work, the e.m.f. work done on binary zinc alloys has been reviewed, and the lanthanum-zinc system, for which no e.m.f. data appear to have been published, was experimentally investigated. The phase diagram for this system has been established by Vogel, Rolla, Iandelli and Canneri⁹⁷. Schramm⁹⁸ also studied this diagram, but only in its zinc-rich part. Pascal²⁴ and Hansen and Anderko⁹⁹ point out that there is disagreement on the stoichiometry of the solid compound in equilibrium with the solution in the zinc-rich part of the diagram. According to Vogel et al.⁹⁷, this would be LaZn_{13} , whereas Schramm⁹⁸ gives the formula LaZn_{11} . Veleckis et al.¹⁰⁰ report the existence of both these compounds. For the purpose of this thesis the formula LaZn_{11} will be assumed; the results are actually unchanged as long as the formula includes one lanthanum atom. The aim of this investigation was to study the saturated lanthanum-zinc solution in

the zinc-rich portion of the diagram, between 430°C and 600°C, by measuring the electromotive force of the cell: $(-)\text{La(s)}/\text{LiCl-KCl(eutectic)}-\text{LaCl}_3/\text{La-Zn(saturated liquid alloy)}(+)$. Experiments were also made to establish the standard potential of the $\text{La(III)}/\text{La(0)}$ electrode in the fused LiCl-KCl eutectic at 450°C. This potential has been determined only once¹⁰¹ and in a higher temperature range (480-550°C); the value calculated by Plambeck¹⁰² at 450° is extrapolated from that data.

I-7. Review of e.m.f. studies of binary zinc alloys

These studies are discussed in some detail for each group of the periodic chart and summarized in Table 1. Indications on phase diagrams given, when necessary, are taken from Pascal²⁴ and Hansen and Anderko⁹⁹, and no attempt has been made to review the data on the diagrams themselves, except when these diagrams have been calculated from e.m.f. measurements.

I-7-1. Alloys of group I-A elements with zinc

None of these alloys appears to have been studied by e.m.f. methods. Experimental difficulties are involved with alkali metals: a solvent such as the eutectic LiCl-KCl , for example, is decomposed by all these metals except Li. Metallic solutions of alkali metals have, however, been studied, using solid electrolytes (glasses)⁴³.

I-7-2. Alloys of group I-B metals with zinc

The copper-zinc phase diagram shows a variety of solid intermetallic phases, which have been studied by Ölander ¹⁰³ from the e.m.f. of the cells: $\text{Zn(l or s)}/\text{LiCl-RbCl(eutectic)}-\text{ZnCl}_2/\text{Zn-Cu(s)}$. This author investigated the entire region below the solidus, between 330 and 600°C and for $x_{\text{Zn}} = 0.42$ to 0.95. This involves the solid phases α , β , β' , γ , δ , ϵ , η and some regions where two of these coexist.

The silver-zinc phase diagram is very similar to the copper-zinc diagram, with solid phases α , β , γ , ϵ , ζ , η . The e.m.f. of the cells: $\text{Zn(l)}/\text{LiCl-KCl(eutectic)}-\text{ZnCl}_2/\text{Ag-Zn(l or s)}$, has been studied, between 428 and 700°C, and for $x_{\text{Zn}} = 0.28$ to 0.84 ^{104,105}. This involves, below the solidus curves, the α , β , γ , and ϵ phases and regions where two of these coexist, and some regions above the solidus.

A partial e.m.f. work on the gold-zinc system has been made ¹⁰⁶. It involves the β' solid phase, between 380 and 550°C, for $x_{\text{Zn}} = 0.44$ to 0.55, and the cells under investigation are: $\text{Zn(l or s)}/\text{LiCl-KCl(eutectic)}-\text{ZnCl}_2/\text{Au-Zn(s)}$.

I-7-3. Alloys of group II-A metals with zinc

Practically nothing was known of the beryllium-zinc system before the work by Dubinin et al.⁵², who studied the e.m.f. of the cell: $\text{Be(s)}/\text{LiCl-KCl(eutectic)}-\text{BeF}_2/\text{Be-Zn(l)}$, between 590 and 790°C and for $x_{\text{Be}} = 10^{-5}$ to 10^{-2} . A small part of the liquidus was thus established; the e.m.f. for saturated solutions being zero, the authors conclude that no intermetallic Be-Zn compounds exist.

E.m.f. studies of magnesium-zinc liquid alloys, involving the cells: $\text{Mg(s)}/\text{LiBr-KBr(eutectic)}-\text{MgBr}_2/\text{Mg-Zn(l)}$ have been made¹⁰⁷, below the melting point of magnesium (650°C) and for $x_{\text{Zn}} = 0.03$ to 0.9. Thermodynamic data are extrapolated at 650°C. Eremenko and Lukashenko¹⁰⁸ use a different electrolyte in their cells, the LiCl-KCl eutectic, but their work on the Mg-Zn system, on a similar temperature and composition range, confirms the data of Terpilowski¹⁰⁷.

As in the case of alkali metals, no e.m.f. data seem to have been published for the alkaline earths-zinc alloys.

I-7-4. Alloys of zinc with other group II-B metals

Cadmium-zinc alloys have been studied by Taylor¹⁴, between 430 and 570°C and for $x_{\text{Zn}} = 0.15$ to 0.85, from the e.m.f. of the cell: $\text{Zn(l)}/\text{LiCl-KCl(eutectic)}-$

$\text{ZnCl}_2/\text{Cd-Zn(l)}$. Lumsden ⁶³ contends that these measurements involve some error, owing to the closeness of the electrode potentials of Cd and Zn. Another e.m.f. study on these alloys has been made by Wynnemer ¹⁰⁹ in a higher temperature range (700-900°C).

Zinc amalgams have been the object of many e.m.f. works ¹¹⁰⁻¹¹⁶. These, however, cover only a small domain, between 18 and 30°C and for x_{Zn} going up to 0.06. In the work of Pearce and Eversole ¹¹⁵, the reference electrode was the most dilute amalgam, and the electrolyte was an aqueous solution of zinc sulphate. Clayton and Vosburgh ¹¹⁶, confirming the data of Cohen ¹¹¹, report at 25°C a zero potential for the saturated amalgam against zinc.

I-7-5. Alloys of group III-B elements with zinc

No e.m.f. studies appear to have been made on the boron-zinc system. The aluminum-zinc system, which presents a eutectic with solid solubility, has been studied extensively by e.m.f. methods by Hilliard et al. ¹¹⁷; the cells used were of the type: $\text{Al(s)}/\text{AlCl}_3\text{-NaCl(equimolecular)}/\text{Al-Zn(l or s)}$, between 320 and 520°C and for $x_{\text{Zn}} = 0.1$ to 0.9. This covered the domains of stability of the α and α' phases, the $\alpha' + \beta$ domain, and some liquid solutions. The work of Eremenko ¹¹⁸ on this system involves cells of the type: $\text{Al(l)}/\text{NaCl-KCl(eutectic)-AlCl}_3/$

Al-Zn(l), between 670 and 850°C and for $x_{\text{Zn}} = 0.14$ to 0.95.

The e.m.f. of the cell: Zn(l)/LiCl-KCl(eutectic)-ZnCl₂/Ga-Zn(l) has been measured ¹¹⁹ between 450 and 545°C and for $x_{\text{Zn}} = 0.04$ to 0.96.

The e.m.f. of the cells Zn(l or s)/LiCl-KCl(eutectic)-ZnCl₂/In-Zn(l) have been measured ¹²⁰ between 360 and 520°C and for $x_{\text{Zn}} = 0.1$ to 0.9.

Kleppa ⁶¹ reports unsatisfactory attempts to study thallium-zinc alloys by e.m.f. methods, due to the closeness of the electrode potentials of the two metals.

I-7-6. Alloys of group IV-B elements with zinc

No e.m.f. studies appear to have been made on the alloys of the first three elements of this column with zinc.

The tin-zinc system has been studied by Taylor ¹⁴ from the e.m.f. of the cell: Zn(l)/LiCl-KCl(eutectic)-ZnCl₂/Sn-Zn(l), between 430 and 570°C, and for: $x_{\text{Zn}} = 0.1$ to 0.9. The measurements of Fiorani and Valenti ¹²¹, on the same cell, between 445 and 550°C, and the e.m.f. results of Sano et al. ¹²² are in good agreement with the study of Taylor ¹⁴. The results of this study were used by Dunkerley and Mills ²³ to the calculation of the tin-zinc phase diagram, which is of

the simple eutectic type, according to the above described method. As has already been mentioned, there was agreement with the previously published diagrams⁵³⁻⁵⁵. About the tin-zinc system, one can also mention the work of Cleveland et al.¹²³, on the same cell, between 450 and 650°C, but for $x_{\text{Zn}} = 0.026$ to 0.12 only, in good agreement with the above mentioned authors.

The lead-zinc system was studied by Kleppa⁶¹, from the e.m.f. of the cell: $\text{Zn(l)}/\text{LiCl-KCl(eutectic)}-\text{ZnCl}_2/\text{Pb-Zn(l)}$, between 420 and 650°C and for $x_{\text{Zn}} = 0.04$ to 0.99. Rosenthal et al.⁶² studied the same cell between 400 and 650°C and for the same composition range. Their data are in very good agreement with the work of Kleppa⁶¹. Rosenthal et al.⁶² used their e.m.f. data for the calculation of the Pb-Zn phase diagram, which presents a miscibility gap in the liquid phase, by a method comparable to the above described method for a diagram with a simple eutectic. The monotectic existing on the zinc-rich side and the eutectic existing on the lead-rich side were in agreement with previous data^{63, 123-126}. As for the shape of the equilibrium curve between the two liquids, it is not in agreement with some of the above authors^{123, 126}.

I-7-7. Alloys of group V-B elements with zinc

No e.m.f. studies appear to have been made on the alloys of the first three elements of this column with zinc.

Seltz ^{47,127} measured the e.m.f. of the cell:

$\text{Zn(l or s)}/\text{LiCl-KCl(eutectic)}-\text{ZnCl}_2/\text{Sb-Zn(l)}$ between 370 and 630°C, and for $x_{\text{Zn}} = 0.1$ to 0.9. The thermodynamic properties of the solid intermetallic compounds ZnSb , Zn_4Sb_3 , Zn_3Sb_2 are calculated from these measurements.

The bismuth-zinc system was studied by Kleppa ⁶¹ from the e.m.f. of the cell: $\text{Zn(l)}/\text{LiCl-KCl(eutectic)}-\text{ZnCl}_2/\text{Bi-Zn(l)}$, between 420 and 600°C and for $x_{\text{Zn}} = 0.06$ to 0.97; Lantratov and Tsarenko ¹²⁸ also report e.m.f. data for this system, between 420 and 800°C and for $x_{\text{Zn}} = 0.14$ to 0.97. As in the lead-zinc case, these data give some information on the liquid miscibility gap in this system. The equilibrium curve between the two liquids, calculated by Kleppa ⁶¹, is not in agreement with the previous works of Haas and Jellinek ¹²⁹ and Spring and Romanoff ¹³⁰, but are in good agreement with some other authors ¹³¹⁻¹³³.

I-7-8. Alloys of rare earth and transition metals with zinc

Only the Y-Zn, La-Zn, Ce-Zn, Er-Zn and U-Zn systems have been studied by e.m.f. methods, in the respective

TABLE 1

Published e.m.f. studies on binary zinc alloys

<u>Solute</u>	<u>Temp. (°C)</u>	<u>Types of cells</u>	<u>Ref.</u>
Ag	430-700	$\text{Zn(l)}/\text{LiCl-KCl(eut.)}-\text{ZnCl}_2/\text{Ag-Zn(l or s)}$	104, 105
Al	320-520	$\text{Al(s)}/\text{AlCl}_3\text{-NaCl(equim.)}/\text{Al-Zn(l or s)}$	117
	670-850	$\text{Al(l)}/\text{NaCl-KCl(eut.)}-\text{AlCl}_3/\text{Al-Zn(l)}$	118
Au	380-550	$\text{Zn(l or s)}/\text{LiCl-KCl(eut.)}-\text{ZnCl}/\text{Au-Zn(s)}$	106
Be	590-790	$\text{Be(s)}/\text{LiCl-KCl(eut.)}-\text{BeF}_2/\text{Be-Zn(l)}$	52
Bi	420-600	$\text{Zn(l)}/\text{LiCl-KCl(eut.)}-\text{ZnCl}_2/\text{Bi-Zn(l)}$	61
	420-800	?	128
Cd	430-570	$\text{Zn(l)}/\text{LiCl-KCl(eut.)}-\text{ZnCl}_2/\text{Cd-Zn(l)}$	14
	700-900	?	109
Ce	400-550	$\text{Ce(s)}/\text{LiCl-KCl(eut.)}-\text{CeCl}_3/\text{Ce-Zn(l)}$	134
Cu	330-600	$\text{Zn(l or s)}/\text{LiCl-RbCl(eut.)}-\text{ZnCl}_2/\text{Zn-Cu(s)}$	103
Er	500-700	$\text{Er(s)}/\text{LiCl-KCl(eut.)}-\text{ErCl}_3/\text{Er-Zn(l)}$	134
Ga	450-545	$\text{Zn(l or s)}/\text{LiCl-KCl(eut.)}-\text{ZnCl}_2/\text{Ga-Zn(l)}$	119
Hg	18-30	$\text{Zn-Hg(l)}_1/\text{ZnSO}_4 \text{ in } \text{H}_2\text{O}/\text{Zn-Hg(l)}_2$ or: $\text{Zn}/\text{ZnSO}_4 \text{ in } \text{H}_2\text{O}/\text{Zn-Hg(l)}$	110-116
In	360-520	$\text{Zn(l or s)}/\text{LiCl-KCl(eut.)}-\text{ZnCl}_2/\text{In-Zn(l)}$	120
La	430-600	$\text{La(s)}/\text{LiCl-KCl(eut.)}-\text{LaCl}_3/\text{La-Zn(l)}$	This work, 134
Mg	420-650	$\text{Mg(s)}/\text{LiBr-KBr(eut.)}-\text{MgBr}_2/\text{Mg-Zn(l)}$	107
	420-650	$\text{Mg(s)}/\text{LiCl-KCl(eut.)}-\text{MgCl}_2/\text{Mg-Zn(l)}$	108
Pb	420-650	$\text{Zn(l)}/\text{LiCl-KCl(eut.)}-\text{ZnCl}_2/\text{Pb-Zn(l)}$	61,62
Sb	370-630	$\text{Zn(l or s)}/\text{LiCl-KCl(eut.)}-\text{ZnCl}_2/\text{Sb-Zn(l)}$	47, 127
Sn	430-650	$\text{Zn(l)}/\text{LiCl-KCl(eut.)}-\text{ZnCl}_2/\text{Sn-Zn(l)}$	14, 121-123
Tl		No stable e.m.f. in this system	61
U	420-850	$\text{U(s)}/\text{LiCl-KCl(eut.)}-\text{UCl}_3/\text{U-Zn(l)}$	48, 49, 89
Y	450-600	$\text{Y(s)}/\text{LiCl-KCl(eut.)}-\text{YCl}_3/\text{Y-Zn(l)}$	95

temperature ranges: 450-500, 430-600, 400-550, 500-700, and 400-850°C, in zinc-rich solutions up to saturation ⁹⁵, this work, ^{134,96,48,49,89}. M being one of these metals, the cells used were of the type: M(s)/LiCl-KCl(eutectic)-MCl₃/M-Zn(l). The saturated solutions with Y, La, Ce and U are in equilibrium with intermetallic compounds which are probably: YZn₁₁, LaZn₁₁, CeZn₁₁ and U₂Zn₁₇ ^{94,97,98,100,135,136}. The work of Hoshino and Plambeck ⁹⁵ on Y-Zn gives data roughly in agreement with those of Chiotti et al. ⁹⁴. The present work on La-Zn is in agreement with the unpublished data of Johnson ¹³⁴. The work by Hoshino and Plambeck on the U-Zn ⁴⁸ system is in good agreement with e.m.f. studies ^{49,89} and other studies ¹³⁶.

The e.m.f.'s for the saturated solutions of Y, La and Ce are, respectively, at 450°, for Y, La, and Ce 0.708, 0.850 and 0.762 volts, which seems to indicate that the properties of the intermetallic compounds in equilibrium with the liquid, probably YZn₁₁, LaZn₁₁ and CeZn₁₁, are quite similar.

II - EXPERIMENTAL

II-1 Apparatus (Fig. 6)

The glassware apparatus used was Pyrex and similar to that used in previous electrode potential studies in molten salts¹³⁷⁻¹³⁹ and alloy studies by e.m.f. methods involving molten salts^{48-52,89-91,96}. The crucible containing the molten salt was a flat-bottomed glass tube. It was contained in an envelope which consisted of a round-bottomed glass cylinder on the wall of which was blown a vacuum-cup stopcock (Corning 7544) connected to a vacuum line. This envelope was closed to the atmosphere by means of a Pyrex cap connected to it with a 75-mm O-ring joint. On this cap were blown five 14/20 female ground-glass joints which were used to insert the thermocouple well, gas inlet, gas outlet, and the electrodes in the cell. All these were such that the inside of the envelope could be isolated from the outer atmosphere or maintained under vacuum when they had been introduced. This vacuum, of 10^{-2} to 10^{-4} torr, was maintained inside the envelope by a mercury diffusion pump in series with a mechanical pump.

The thermocouple well consisted of 5-mm glass tubing closed at its lower end, which was below the melt surface, and connected at its upper end to a 14/20 male ground glass joint. The gas inlet consisted of 5 mm

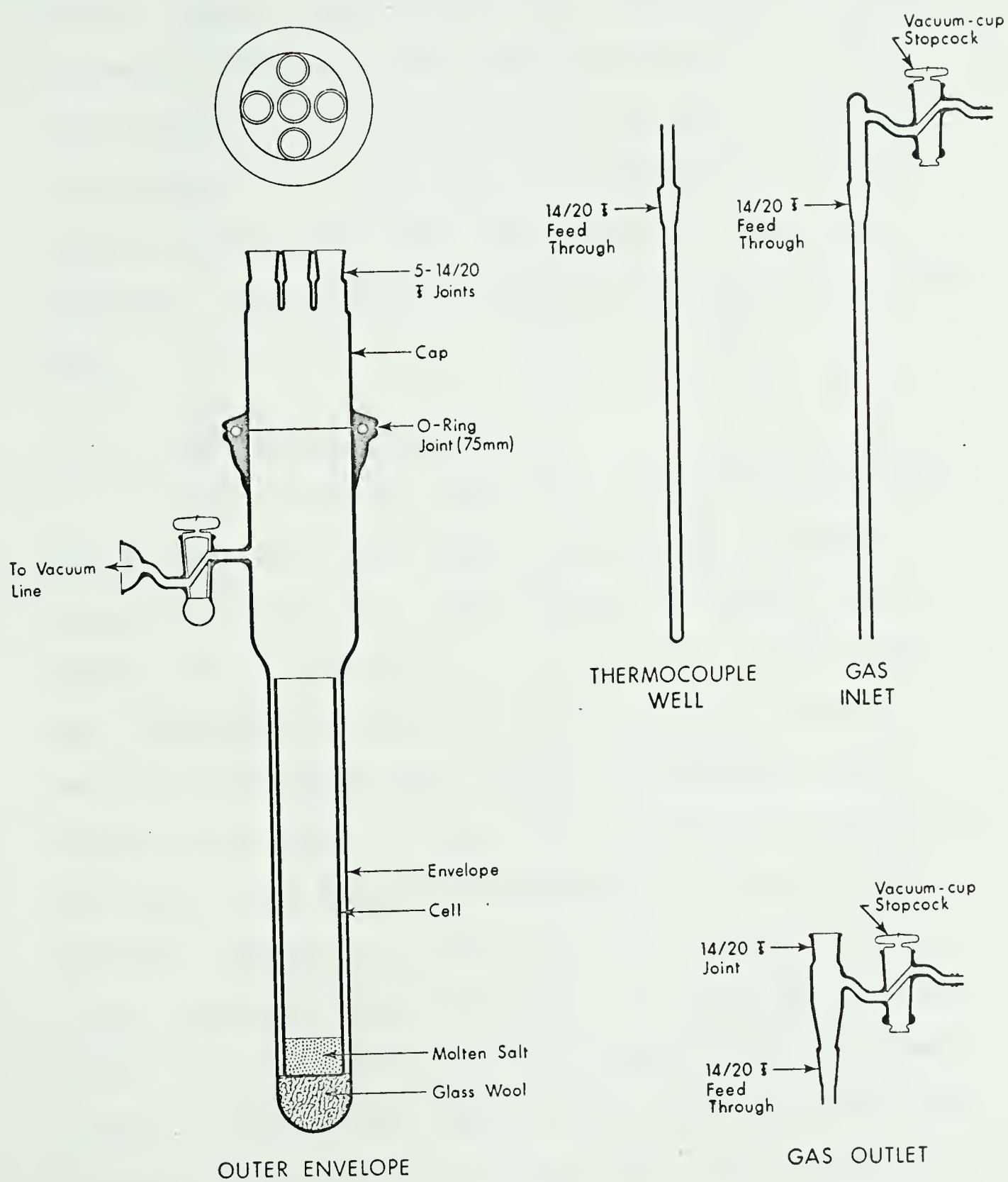


Figure 6. Glassware apparatus.

glass tubing connected to a 14/20 male ground-glass joint, sealed at its top, on the side of which was blown a vacuum-cup stopcock. Its lower end was above the melt. The gas outlet was a male 14/20 ground-glass joint on the side of which was blown a vacuum-cup stopcock; its upper end was connected to a 14/20 female ground-glass joint into which the inlet was inserted. The outlet was inserted in one of the 14/20 joints of the cap.

II-2. Electrodes (Fig. 7)

In the lanthanum electrode potential measurements, three electrodes were used: a lanthanum electrode, which was a 1/8" dia. and 5" length lanthanum rod (A.D. Mackay, Inc., New York, N.Y.) to which a copper lead was attached well above the melt level; a platinum reference electrode and a counter-electrode, each of which consisted of a large platinum flag (platinum wire and sheet from Engelhard Industries of Canada, Ltd., Toronto) welded to a copper lead and sealed to a 5-mm glass insulation tube below the lower end of the lead. These three electrodes were introduced in compartments made of a 12-mm glass tube closed with a fritted glass disc of porosity D or E (Ace Glass, Inc., Vineland, N.J.). The bulk of the melt acted as a salt bridge.

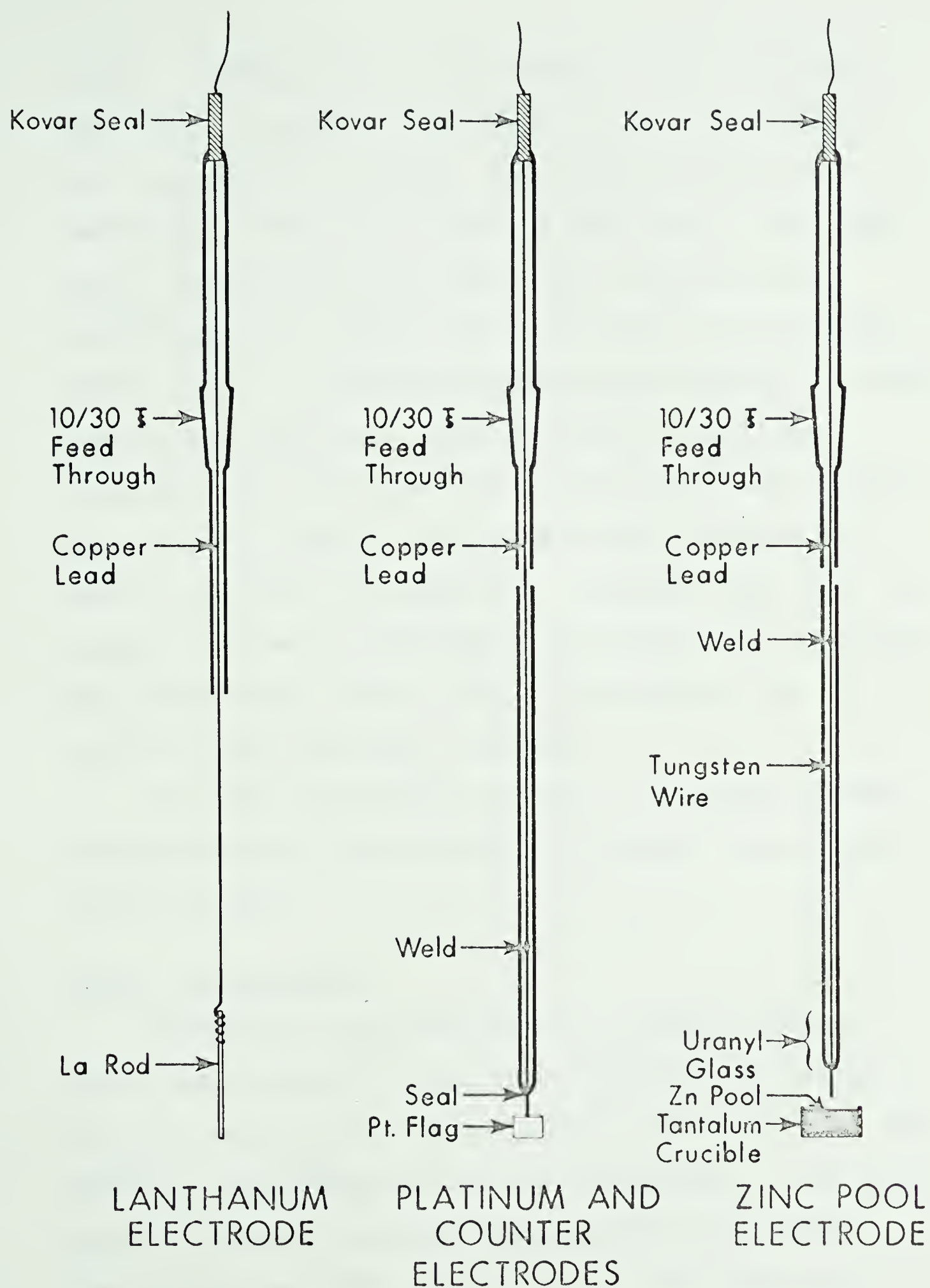


Figure 7. Electrodes.

In the lanthanum-zinc alloy studies, two electrodes were used: a lanthanum electrode, as described above, and a zinc pool electrode. The liquid zinc was contained in a tantalum crucible on the bottom of the cell tube. Contact to it was made with a tungsten wire (0.020" dia; A.D. Mackay, Inc., New York, N.Y.) dipped in the liquid zinc at its lower end and welded to a copper lead at its upper end; this wire and the lead were insulated with 5-mm glass tubing, the lower end of which, made of uranyl glass, was sealed to the tungsten wire about 1 cm above its lower end. At their upper end, the copper leads were sealed through a Kovar seal to a 10/30 male feedthrough which could be inserted in one of the joints of the cap using a reducer.

To avoid thermocouple effects, connections between different metals were all made in the hot central region of the furnace.

II-3. Instruments

Potentials were measured with a Hewlett-Packard Model 3400A digital voltmeter. A Model IV coulometric current source (E.H. Sargent and Co., Chicago, Ill.) was used for electrodepositions and anodizations. The bottom part of the cell envelope was inserted in a Lindberg Hevi-Duty Type 54381A furnace with a Type 59344 temperature control unit. A constant temperature could be

maintained in the cell within 1°C. Temperatures were measured with a chromel-alumel thermocouple calibrated at the zinc melting point. The thermocouple e.m.f. was measured with the digital voltmeter.

II-4. Preparation of molten salt

A modification of the method of Maricle and Hume⁴² was used. The anhydrous, crystalline, reagent grade lithium and potassium chlorides (The McArthur Chemical Co., Ltd., Montreal) were mixed thoroughly in eutectic proportions. About one mole percent anhydrous lanthanum trichloride (A.D. Mackay, Inc., New York, N.Y.) was added in the case of the lanthanum-zinc alloy experiments. The mixture was progressively heated under vacuum (10^{-3} to 10^{-4} torr) to 450°C and maintained under these conditions for twelve hours in the crucible and envelope previously described. Then argon was introduced in this envelope and the crucible transferred to a Hevi-Duty Model 80 furnace under the fume hood where chlorine was bubbled through the melt for one hour. Argon was bubbled through for four to six hours to remove the chlorine. The melt was then poured into glass tubes that were sealed under argon for storage of the frozen melt.

II-5. Preparation of lanthanum-zinc alloys

About twenty grams of reagent grade zinc shot (May

and Baker Ltd., Dagenham, Essex, England) were melted in a small glass tube under zinc chloride. The zinc piece obtained was carefully washed, dried and polished in order to eliminate surface zinc oxide and chloride. It was then cut into smaller pieces and introduced in a 1" O.D. x 7/16" deep tantalum crucible (A.D. Mackay, Inc., New York, N.Y.) together with several previously polished small pieces of lanthanum weighing from 0.3 g to 1.0 g. The crucible was then set on the bottom of the glass envelope described above, under a flow of argon at 500°C, for fifteen to twenty hours. The piece of alloy was easily removed from the crucible after cooling down, owing to its contraction, then carefully polished and stored until use.

II-6. Procedure

A tube of purified melt was opened. The salt was introduced in the cell under argon and maintained under vacuum (10^{-3} to 10^{-4} torr) at 400°C for twelve hours. Then argon was introduced while the electrode system was set up. This argon was purified by successive passage over hot copper, magnesium perchlorate, titanium sponge at 900°C (the use of a titanium sponge as a nitrogen adsorbent has been described previously¹⁴⁰) and magnesium perchlorate. The cell was put under vacuum again. In the La(III)/La(0) electrode potential measurements, the

platinum reference electrode was first anodized until a mole fraction of 5×10^{-4} to 10^{-3} in Pt(II) was reached in the corresponding compartment. Similarly, mole fractions of La(III) from 10^{-4} to 3×10^{-3} were obtained in successive generations in the lanthanum compartment. After each generation, the lanthanum electrode was rotated in order to obtain a homogeneous concentration of La(III) in the compartment rapidly. Its potential against the platinum reference and the temperature were then taken as a function of time. The mole fractions of ions in the compartments were calculated from the total number of equivalents generated and the total number of equivalents of chloride in these compartments, obtained by Mohr titration as previously described¹⁴¹.

In the lanthanum-zinc alloy experiments, the potential of the zinc pool against the lanthanum electrode and the temperature were measured as a function of time. Then the temperature was changed and another point taken. It appeared that no more than two points could be taken in a given experiment. This was true even for evacuated apparatus which, nevertheless, behaved better than that held under a positive pressure of purified argon. However, similar difficulties have been encountered previously, and might be ascribed to apparatus corrosion tending to remove the lanthanum

from the alloy ⁹⁰, and/or to a poor contact with the tungsten lead caused by surface oxide formation.

All calculations were carried out on the University of Alberta I.B.M. 360 computer. The programs used are given in the appendix. Error limits given are the 95% confidence limits, with the hypothesis of a normal distribution of the errors.

III- RESULTS AND DISCUSSION

III-1. Standard potential of La(III)/La(0)

After elimination of questionable points, usually at lower concentrations range, 36 data points obtained in six different experiments (numbered runs 1 to 6 in appendix) were used. Potentials were measured as a function of La(III) concentration at a constant temperature. The time necessary to reach equilibrium varied from 5 to 30 minutes, the potential at equilibrium being constant with random variations of less than 2 mV/15 minutes, due to temperature fluctuations. Potentials at equilibrium were averaged over these small variations. Temperatures at equilibrium were also averaged for small fluctuations, usually of the order of 1°C. For all experiments the mean e.m.f. values were corrected to correspond to a standard electrode of unit mole fraction Pt(II) (S.M.F.P.E.) as a reference using the mean temperatures for each e.m.f.-concentration point; the platinum electrode is known to obey the Nernst equation with a two-electron process ¹⁴¹. Plots of these e.m.f. values against the logarithm of the mole fraction of La(III) in the lanthanum compartment were linear (Fig. 8) showing that the lanthanum electrode is Nernstian in this solvent. For each run, the slope and the intercept of the straight lines representing

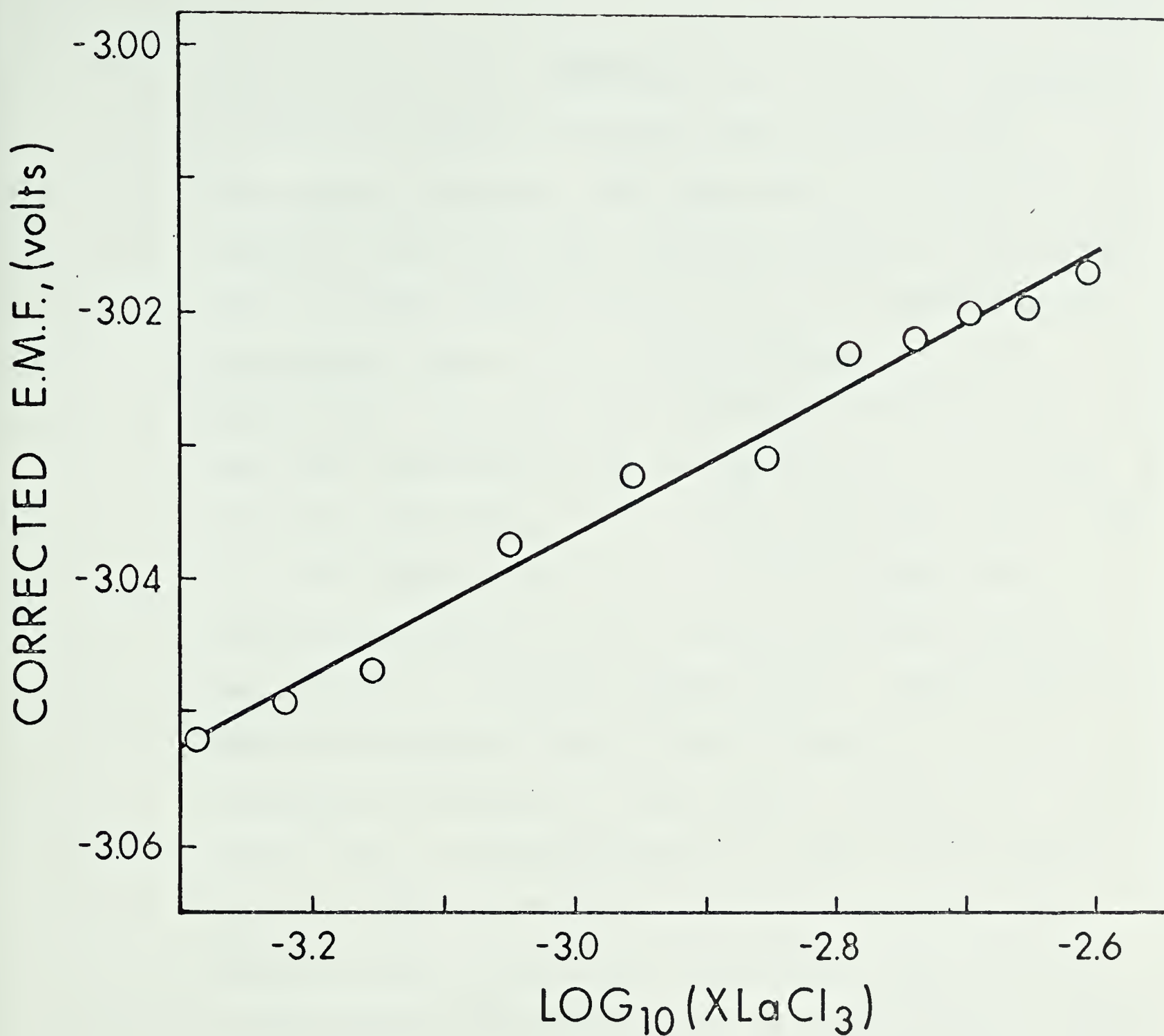


Figure 8.

Nernstian plot for the potential of the $\text{La(III)}/\text{La(0)}$ couple in LiCl-KCl eutectic, corrected to S.M.F.P.E., for a typical experiment (run no. 3, 447.4°C).

the variation of the corrected e.m.f. with the logarithm of the mole fraction of La(III) were calculated by least square analysis. The mean number of electrons involved in the lanthanum electrode process as calculated from the Nernst slopes was 3.0 ± 0.7 , in agreement with the expected value of 3. One experiment gave only a single point, for which the intercept was calculated using the theoretical slope of the line for a trivalent lanthanum electrode process. These intercepts give a set of values (Table 2 and Fig. 9) of the standard mole fraction potentials of the lanthanum electrode against the S.M.F.P.E. at various temperatures. Linear interpolation (fitting by least square analysis the best straight line through the experimental temperature - e.m.f. points) gave a standard potential of the La(III)/La(0) couple at 450°C of -2.883 ± 0.007 volts, on the mole fraction scale. The values obtained for this potential on the molarity and molality scales at 450°C were -2.848 and -2.853 volts, respectively, with the same precision. The temperature coefficient obtained was 4.4×10^{-4} volts/°C with a standard error of 2×10^{-4} volts/°C. Using the data of Laitinen and Pankey¹³⁷ for the chlorine electrode against Pt(II) and the data of Yang and Hudson¹⁰¹ for the lanthanum electrode against Cl_2/Cl^- , Plambeck¹⁰² calculated, at 450°C, a standard potential for a lanthanum

TABLE 2

Standard potential of the La(III)/La(0) couple
against S.M.F.P.E. as a function of temperature

<u>Mean temp. (°C)</u>	<u>Standard potential (V)</u>
430.5	-2.886
446.3	-2.883
447.4	-2.877
450.5	-2.895
478.6	-2.873
545.2	-2.839

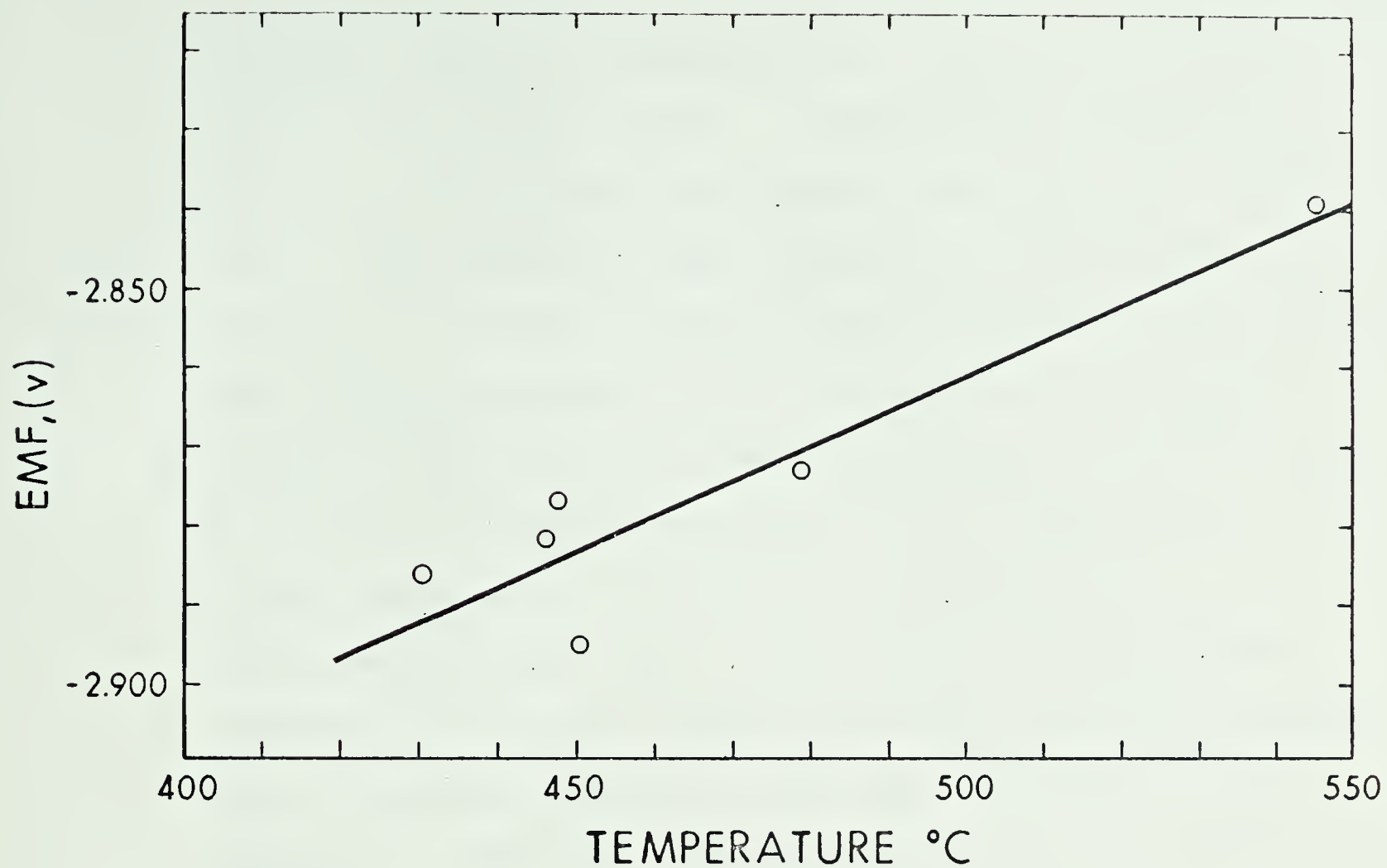


Figure 9. Standard potential of the La(III)/La(O) couple in LiCl-KCl eutectic, against S.M.F.P.E., as a function of temperature.

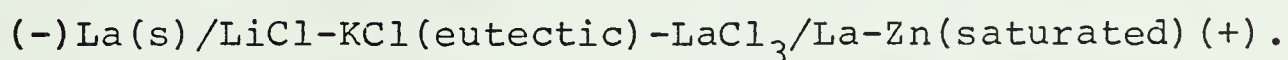
electrode against Pt(II)/Pt(0) of -2.912 ± 0.005 volts, on the mole fraction scale. A temperature coefficient of 6.4×10^{-4} volts/°C can also be calculated from these data. The potential value obtained from the present study is 29 mV more positive than the previous value¹⁰². The problems involved in the calculation of potential values at 450°C from the data of Yang and Hudson¹⁰¹ have been discussed by Plambeck^{102,139}; these are higher temperatures (480-550°C), concentrations sufficiently higher than in the present work and other studies^{95,139}, that Henrian behaviour cannot be assumed, and a different reference electrode. Plambeck¹⁰² also points out that only a few experimental points are given for each couple (ten for La(III)/La(0)). In a study of the very similar Y(III)/Y(0) couple, Hoshino and Plambeck⁹⁵ also find electrode potentials about 30 mV higher than those calculated from the data of Yang and Hudson.

In this work, the temperature coefficient is not known accurately. It agrees satisfactorily with the value calculated from previous experiments in that this value falls in the range of the rather large experimental error.

III-2. Liquid La-Zn alloy

The equation given by Johnson and Dillon⁹¹ for the solubility of lanthanum in liquid zinc (in g/kg):
 $\log w = 9.573 - 8718/T$ gives a very low solubility

of lanthanum in zinc in the range 430-600°C (2.0×10^{-2} g/kg at 500°C). It was not possible to prepare unsaturated solutions for study due to the extremely small quantities of lanthanum required for saturation. Attempts to prepare the saturated solutions by electrodeposition of lanthanum or by using a quantity of lanthanum slightly in excess of the reported saturation level failed; higher (from 0.95 to 1.20 volts) and less stable (within 10 mV or more) cell potentials than those reported below were observed, possibly corresponding to unsaturated solutions. It was found necessary to take a large excess of lanthanum (1 to 5% by weight) to obtain the saturated solution. The results discussed here are independent of further addition of lanthanum (by electrodeposition on the zinc pool). This shows that saturation had been reached, with the excess lanthanum forming an intermetallic compound, assumed here to be LaZn_{11} . Therefore at each temperature point, the e.m.f. obtained was that of the cell:



A time varying from one to six hours was found necessary to reach equilibrium, the potential at equilibrium being constant with variations of less than 0.5 mV/30 min in most cases. Potentials at equilibrium were averaged for these small variations. Temperatures were constant within 1°C as in the $\text{La(III)}/\text{La(0)}$ potential experiments and were similarly averaged. Thus a set of mean temperature-e.m.f. values was obtained (Table 3). The best straight

TABLE 3E.m.f. of the cell(-)La/LiCl-KCl(eutectic)-LaCl₃/La-Zn(sat.)(+)as a function of temperature

<u>Mean temp. (°C)</u>	<u>Mean e.m.f. (V)</u>
445.5	0.8584
450.4	0.8474
477.8	0.8368
495.5	0.8052
503.9	0.8014
511.1	0.8103
523.1	0.7947
585.5	0.7479

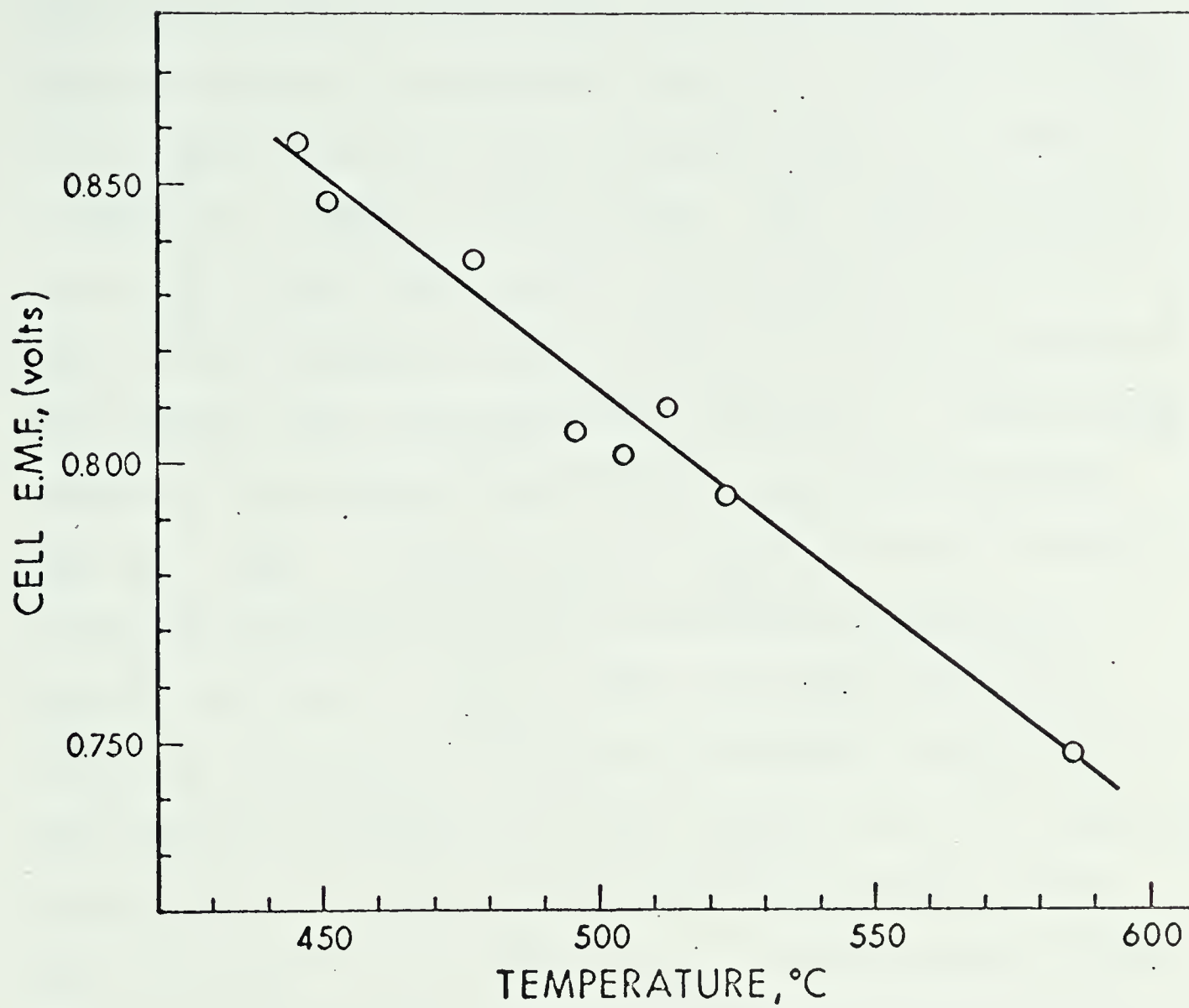


Figure 10. E.m.f. of the cell $(-)\text{La}/\text{LiCl-KCl}(\text{eut-ectic})-\text{LaCl}_3)/\text{La-Zn}(\text{sat.})$ as a function of temperature.

line through these points (Fig. 10) was fitted by least square analysis, its equation being: $E = 1.4085 - 7.71 \times 10^{-4}T$; this is valid in the range 430-600°C and gives, at 450°C, $E = 0.8506 \pm 0.005$ volts. The overall process occurring in the cell amounts to the formation of the pure (solid) compound LaZn_{11} from pure (solid) lanthanum and (liquid) zinc saturated with lanthanum. If ΔG is the change in free energy involved, it can be easily seen that $\Delta G = g_{\text{La}}^m + 11(\mu_{\text{Zn}}(\text{LaZn}_{11}) - \mu_{\text{Zn}}(l))$; since, in the liquid-solid phase equilibrium involved: $\mu_{\text{Zn}}(\text{LaZn}_{11}) = \mu_{\text{Zn}}(l)$, one has $\Delta G = g_{\text{La}}^m = -nFE$. Let $\Delta G_f^\circ, \text{LaZn}_{11}(s)$ be the free energy of formation of (solid) LaZn_{11} from pure (solid) lanthanum and pure (liquid) zinc, and a_{Zn} the activity of the zinc in the saturated solution, then $\Delta G_f^\circ, \text{LaZn}_{11}(s) = \Delta G + 11RT \ln a_{\text{Zn}}$. If one assumes ideal behaviour of the zinc, since the solution of lanthanum is very dilute, $a_{\text{Zn}} = 1 - x_{\text{La}}$, where x_{La} is the mole fraction of lanthanum. Then, since x_{La} is very small, $\Delta G_f^\circ, \text{LaZn}_{11}(s) = \Delta G - 11RT x_{\text{La}}$. At 500°C, the term $-11RT x_{\text{La}}$ is -0.177 cal/mole, which is negligible. Thus $\Delta G_f^\circ, \text{LaZn}_{11}(s) = \Delta G$, so that $\Delta G_f^\circ, \text{LaZn}_{11}(s)$ is simply $-nFE$, where $n=3$.

In the same manner, the entropy of formation $\Delta S_f^\circ, \text{LaZn}_{11}(s)$ is $nF(dE/dT)$ and the enthalpy formation $\Delta H_f^\circ, \text{LaZn}_{11}(s)$ can be calculated by extrapolating the free

energy to 0°K. At 450°C for ΔG_f° , $\text{LaZn}_{11}(\text{s})$ and over the temperature range 430–600°C for the other quantities,

$$\Delta G_f^\circ, \text{LaZn}_{11}(\text{s}) = -58.8 \pm 0.6 \text{ kcal/mole}$$

$$\Delta S_f^\circ, \text{LaZn}_{11}(\text{s}) = -53.4 \pm 8.0 \text{ cal/deg. mole}$$

$$\Delta H_f^\circ, \text{LaZn}_{11}(\text{s}) = -97.4 \pm 6.0 \text{ kcal/mole .}$$

In addition, ΔG_f° , $\text{LaZn}_{11}(\text{s})$ was calculated at temperatures ranging from 430 to 600°C (Table 4), from the equation $\Delta G_f^\circ, \text{LaZn}_{11}(\text{s}) = -97.415 + 5.335 \times 10^{-2}T$, where T is in °K. It appears that these e.m.f. values differ from those obtained in a similar experiment by Johnson¹³⁴ by at most 2%. The discrepancies are somewhat greater for the entropy and enthalpy.

TABLE 4

Calculated free energy of formation of LaZn_{11}

as a function of temperature

Temp. ($^{\circ}\text{C}$)	$\Delta G_f^{\circ}, \text{LaZn}_{11}$ <u>(Kcal/mole).</u>
430	-59.9
450	-58.8
500	-56.2
550	-53.5
600	-50.8

IV - C O N C L U S I O N

The thermodynamic theories examined in the introduction provide a satisfactory basis for experimental studies of alloys by e.m.f. methods. It should be noted, however, that, especially in multicomponent systems, their application requires a fair amount of work, in both experiment and computations from experimental data, but the results thus obtained are rigorous. The use of a solution model reduces this work substantially, but the results obtained are only a rough approximation, especially at high concentrations.

From the experimental part of this work, a value for the standard potential of the La(III)/La(0) couple at 450°C was calculated; the thermodynamic data computed for the compound in equilibrium with the liquid saturated lanthanum-zinc solution should be a useful contribution to the knowledge of the properties of the lanthanum-zinc system, which is still only partial.

Regarding possible practical applications in spent nuclear fuel processing, it should be noticed that the compound LaZn_{11} appears from this study to be of much greater stability than $\text{UZn}_{8.5}$; the standard energies of formation at 450°C being -58.8 and -26.1 kcal/mole⁴⁸ respectively. The standard potentials of pure uranium and pure lanthanum (any scale since both metals are trivalent) in the LiCl-KCl eutectic melt differ by 0.630 V,

making electrochemical separation of these metals appear quite feasible. Using the free energies given above, the difference in standard potentials of uranium (saturated solution in zinc) and lanthanum (saturated solution in zinc), in the LiCl-KCl eutectic melt, is only 0.156 V at 450°C. The alloying with excess zinc thus appears unfavourable, since it reduces the feasibility of separating these elements electrochemically by a significant factor.

Since most rare earth metals are fission impurities^{92,93}, it might be desirable to study other rare earth-zinc systems as has been done here for the lanthanum-zinc system. Rare earth metals having very similar properties, it is likely that the same conclusion as here would be reached. This is confirmed by already existing data for the yttrium-zinc system^{94,95}, and on the Y(III)/Y(0) electrode potential in the LiCl-KCl eutectic^{95,101,102}, and for the cerium-zinc and erbium-zinc systems⁹⁶.

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VI - A P P E N D I X

Here follow the IBM 360 FORTRAN IV programs used in calculations from experimental data, according to the output given by the University of Alberta IBM 360 computer.


```

C .....
C MAINLINE FOR CALCULATION OF STANDARD POTENTIALS FROM NERNST EQUATION.
C .....
C PURPOSE.
C .....
C THIS PROGRAM CALCULATES THE STANDARD POTENTIAL OF THE METALLIC
C ELECTRODE M IN THE CELL:
C .....
C
C R/R-ION/M-ION/M,
C .....
C WHERE R IS A REFERENCE METALLIC ELECTRODE, IN THE MOLE FRACTION SCALE.
C MEASUREMENTS ARE MADE AT CONSTANT TEMPERATURE, CONSTANT CONCENTRATION
C IN R-ION AND VARIABLE CONCENTRATION IN M-ION. EXPERIMENTAL VALUES ARE
C CORRECTED TO A MOLE FRACTION IN R-ION OF 1, BY MEANS OF NERNST EQUATION.
C THE BEST STRAIGHT LINE REPRESENTING THE VARIATION OF THE CORRECTED EME
C AGAINST THE LOG OF THE MOLE FRACTION OF M-ION IS ESTABLISHED BY LEAST
C SQUARE ANALYSIS, FOR EACH CONSTANT-TEMPERATURE EXPERIMENT. ITS SLOPE GIVES
C THE NUMBER OF ELECTRONS INVOLVED IN THE M-ELECTRODE PROCESS, AND ITS
C INTERCEPT THE STANDARD EME AT THE EXPERIMENTAL TEMPERATURE, WHICH HAS
C BEEN AVERAGED FOR SMALL FLUCTUATIONS. THE CASE WHEN THERE IS ONLY ONE
C TEMPERATURE-EME POINT IN ONE EXPERIMENT IS EXAMINED SEPARATELY.
C THE BEST STRAIGHT LINE REPRESENTING THE TEMPERATURE DEPENDENCE OF THE
C STANDARD POTENTIAL IS ESTABLISHED BY LEAST-SQUARE ANALYSIS. INTERCEPTS
C ARE CALCULATED FOR SEVERAL TEMPERATURE ORIGINS. THE TEMPERATURE CORRECTION
C IS ALSO GIVEN. THE AVERAGE NUMBER OF ELECTRONS INVOLVED IN THE
C M-ELECTRODE PROCESS IS CALCULATED. STANDARD DEVIATIONS ARE CALCULATED
C ON ALL THESE QUANTITIES.
C SEVERAL SUCH PROBLEMS CAN BE TREATED.
C

```



```

C INPUT.
C
C N, P ON ONE CARD FORMAT D16.
C N: NUMBER OF CONSTANT TEMPERATURE EXPERIMENTS.
C P: NUMBER OF ORIGINS FOR TEMPERATURES.
C
C EKR, EKM, ECT, REC ON ONE CARD FORMAT D16.6.
C EKR: NUMBER OF ELECTRONS INVOLVED IN REFERENCE ELECTRODE PROCESS.
C EKM: NUMBER OF ELECTRONS INVOLVED IN WORKING ELECTRODE PROCESS.
C ECT: FACTOR BY WHICH THE INDICATION OF THE COULOMETRIC CURRENT SOURCE
C      USED FOR GENERATING THE ELECTRODES HAS TO BE MULTIPLIED TO OBTAIN
C      MICROEQUIVALENTS.
C ECT: EXPERIMENTAL ERROR ON TEMPERATURES.
C REC: EXPERIMENTAL ERROR ON POTENTIALS.
C
C TITLE ON ONE CARD FORMAT 19A4.
C
C FOR EACH CONSTANT TEMPERATURE EXPERIMENT:
C
C M, COUL, DR, DM, ON ONE CARD FORMAT I6,3D12.6.
C M: NUMBER OF M-ION CONCENTRATION-TEMPERATURE POINTS.
C COUL: INDICATION OF COULOMETRIC CURRENT SOURCE FOR REFERENCE ELECTRODE.
C DR: NUMBER OF MOLES IN REFERENCE COMPARTMENT.
C DM: NUMBER OF MOLES IN WORKING ELECTRODE COMPARTMENT.
C
C M VALUES OF TEMPERATURE PUT IN ARRAY TC, ON M CARDS FORMAT D16.6.
C
C M VALUES OF COULM AND EMF ON M CARDS FORMAT D16.6.
C COULM: INDICATION OF COULOMETRIC CURRENT SOURCE FOR WORKING ELECTRODE.
C
C P VALUES OF ORIGINS FOR TEMPERATURES PUT IN ARRAY TO, ON P CARDS FORMAT D16.6.
C

```



```

C
C OUTPUT.
C
C
C TITLE.
C
C FOR EACH CONSTANT-TEMPERATURE EXPERIMENT:
C NUMBER OF RUN.
C TABLE OF M VALUES OF TEMPERATURE, MOLE FRACTION OF M-ION, LOG MOLE FRACTION OF
C M-ION, CORRECTED EMF.
C AVERAGE TEMPERATURE.
C STANDARD DEVIATION ON AVERAGE TEMPERATURE.
C STANDARD EMF AT AVERAGE TEMPERATURE.
C SLOPE OF NERNSTIAN LINE.
C THEORETICAL SLOPE OF NERNSTIAN LINE.
C STANDARD DEVIATION ON SLOPE OF NERNSTIAN LINE.
C NUMBER OF ELECTRONS INVOLVED IN M-ELECTRODE PROCESS.
C
C FOR EACH ORIGIN OF TEMPERATURES:
C ORIGIN OF TEMPERATURES IN DEGREES C.
C STANDARD EMF AT THIS TEMPERATURE.
C STANDARD DEVIATION ON THIS EMF.
C TEMPERATURE COEFFICIENT OF STANDARD EMF.
C STANDARD DEVIATION ON THIS COEFFICIENT.
C AVERAGE NUMBER OF ELECTRONS INVOLVED IN M-ELECTRODE PROCESS.
C STANDARD DEVIATION ON THIS NUMBER.

```

```

C .....
C
C

```



```

ISN 0002      IMPLICIT REAL*8(A-H,C-Z)
ISN 0003      REAL*8 T(20),TC(20),EMEC(20),YM(20),EMEO(20),FKME(20),TO(5),RS(5),
              PRS(5),FKMES(20)
ISN 0004      REAL TITLE(19)
ISN 0005      INTEGER P

C
C R=(PERFECT GAS CONSTANT)/(FARADAY CONSTANT)*P IN JOULES/DEGREES K, FARADAY
C CONSTANT IN COULOMPS, POTENTIALS IN VOLTS, TEMPERATURES IN DEGREES C OR K,
C MASSES IN MOLES AND CONCENTRATIONS IN MOLE FRACTIONS.
C
ISN 0006      DATA R/ 0.198478107220D-3/

C
C PRELIMINARY READING OF DATA.
C
ISN 0007      I READ(5,100,END=10) N,P,EKR,EKM,FACT,RTC,REC,TITLE
ISN 0008      WRITE(6,101) TITLE
ISN 0009      N1=0

C
C LOOP READS AND PROCESSES DATA FOR EACH OF THE N CONSTANT-TEMPERATURE
C EXPERIMENTS.
C
ISN 0010      DO 4 I=1,N
ISN 0011      READ(5,102) M,COULR,DR,DW

C
C COULR=COULR*FACT
C X2=COULR*1.0D-6/(EKR*DR)

```



```

ISN 0014 YR=DLG10(XR)
ISN 0015 WRITE(6,103) I
ISN 0016 DO 2 J=1,M
ISN 0017 2 READ(5,104) TC(J)
ISN 0018 CALL AVERT(M,TC,TS,RT,PTC)
ISN 0019 T(I)=TS
ISN 0020 DO 3 J=1,M
ISN 0021 READ(5,105) COULM,EMF
ISN 0022 COULM=COULM*EFACT
ISN 0023 XM=COULM*1.00-6/(EKM*DM)
ISN 0024 YM(J)=DLG10(XM)
ISN 0025 EMEC(J)=EMF+R*(TC(J)+0.27316D3)*YR/EKR
ISN 0026 3 WRITE(6,106) TC(J),XM,YM(J),EMEC(J)
ISN 0027 SLT=R*(T(I)+0.27316D3)/EKM

C
C IF M=1 CALCULATION IS NOT APPLICABLE; SUCH A RUN IS ELIMINATED FROM CAL-
C -CULATION OF AVERAGE NUMBER OF ELECTRONS.
C
IF(M.EQ.1) GO TO 9
CALL LEAST(M,YM,EMEC,0.000,SL,EMES,RSL,PE)
EMEO(I)=EMES
EKME(I)=SLT*EKM/SL
NI=NI+1
EKMES(NI)=EKME(I)
4 WRITE(6,107) T(I),RT,EMEO(I),SL,SLT,RSL,PE,EKME(I)
WRITE(6,108)

```



```

ISN 0037      DO 7 I=1,P
ISN 0038      READ(5,109) TO(I)
ISN 0039      IF(I.GT.1) GO TO 5
ISN 0041      CALL LEAST(N,T,EMF0,TO(I),A,B,RA,RB)
ISN 0042      GO TO 6
ISN 0043      5 CALL LEAST(N,T,EMF0,TO(I),B,RB)
ISN 0044      6 RS(I)=R
ISN 0045      7 RRS(I)=RB
ISN 0046      DO 8 I=1,P
ISN 0047      8 WRITE(6,110) TO(I),BS(I),RBS(I)
ISN 0048      WRITE(6,111) A,RA

C
C AVERAGE NUMBER OF ELECTRONS AND STANDARD DEVIATION ON IT ARE CALCULATED.
C
      CALL AVERT(N1,EKME,EKMS,RKM,0.000)
      WRITE(6,112) EKMS,RKM

C
C CONTROL IS TRANSFERRED TO STATEMENT 1 FOR ANOTHER PROBLEM TO BE TREATED.
C
      GO TO 1

C
C IN CASE M=1 STANDARD EMF IS CALCULATED USING THEORETICAL SLOPE OF
C NERNSTIAN LINE. STANDARD DEVIATION IS TAKEN AS EXPERIMENTAL ERROR AND
C NUMBER OF ELECTRONS AS ASSUMED THEORETICAL ONE (FKM).
C
      9 EMF0(I)=EMF0(1)-P*(T(I)+0.27316D3)*VM(1)/RKM

```



```

ISN 0052 T(I)=TC(I)
ISN 0053 SL=SLT
ISN 0054 RE=REC
ISN 0055 RT=RTC
ISN 0056 EKMF(I)=EKM
ISN 0057 GN TO 4
ISN 0058
ISN 0059
ISN 0060
ISN 0061
ISN 0062
ISN 0063
ISN 0064
ISN 0065
ISN 0066
ISN 0067
ISN 0068
ISN 0069
ISN 0070
ISN 0071
ISN 0072
ISN 0073

10 STOP
100 FORMAT(2I6/5D12.6/19A4)
101 FORMAT(1H1,19A4//1H )
102 FORMAT(16,3D12.6)
103 FORMAT(1H // , RUN NO ,14// , TEMPERATURE MOLE FRACTION
1 LOG MOLE FR. CORRECTED EMF ,/1H )
104 FORMAT(D16.6)
105 FORMAT(2D16.6)
106 FORMAT(2D16.6,D20.6,D16.6)
107 FORMAT(1H // TEMPERATURE= ,D16.6// STANDARD DEVIATION ON TEMPERAT
1 UPE= ,D16.6// STANDARD EMF= ,D16.6// SLOPE= ,D16.6// THEORETICAL
2 SLOPE= ,D16.6// STANDARD DEVIATION ON EMF= ,D16.6// STANDARD DE
3 VIATION ON SLOPE= ,D16.6// NUMBER OF ELECTRONS INVOLVED= ,D12.4)
108 FORMAT(1H // )
109 FORMAT(D16.6)
110 FORMAT(1H // , TO= ,D16.6// STANDARD EMF AT TO= ,D16.6// STAND
1 ARD DEVIATION ON EMF AT TO= ,D16.6)
111 FORMAT(1H // , TEMPERATURE COEFFICIENT OF STANDARD EMF= ,D16.6// ,
1 STANDARD DEVIATION ON IT= ,D16.6)
112 FORMAT(1H // , AVERAGE NUMBER OF ELECTRONS INVOLVED= ,D12.4// , ST
1 ANDARD DEVIATION ON IT= ,D12.4)
END

```

***** END OF COMPILATION *****

VI-2. 'ZINC' program used in interpretation of results of

lanthanum-zinc alloy experiments (mainline only)

```

C .....
C MAINLINE FOR THERMODYNAMIC CALCULATIONS FROM EMF DATA.
C
C PURPOSE.
C
C THIS PROGRAM CALCULATES THERMODYNAMIC DATA FOR AN INTERMETALLIC
C COMPOUND OF TWO METALS M1 AND M2 FROM THE EMF OF THE CELL:
C
C M2/SOLUTION OF M2 ION /SATURATED SOLUTION OF M2 IN M1
C
C IT FIRST ESTABLISHES THE TEMPERATURE DEPENDENCE OF THIS EMF ON A LINEAR
C BASIS; INTERCEPT IS CALCULATED FOR SEVERAL REFERENCE TEMPERATURES TAKEN
C AS ORIGINS, THEN IT CALCULATES THE FREE ENERGY AT SEVERAL REFERENCE TEMPE-
C RATURES AND THE ENTROPY AND ENTHALPY, FOR THE FORMATION OF THE COMPOUND
C IN EQUILIBRIUM WITH THE M1-M2 SOLUTION, AND FINALLY THE FREE ENERGY AS A
C FUNCTION OF TEMPERATURE. STANDARD DEVIATIONS ARE CALCULATED ON ALL THESE
C QUANTITIES.
C SEVERAL SUCH PROBLEMS CAN BE TREATED.
C
C INPUT.
C
C N,P,Q ON ONE CARD FORMAT 316.
C N:  NUMBER OF TEMPERATURE-EMF POINTS.
C P:  NUMBER OF REFERENCE TEMPERATURES.
C Q:  NUMBER OF FREE ENERGIES TO BE CALCULATED AS A FUNCTION OF TEMPE-
C      -RATURE.

```



```

C      EK,TA,PAS,RTC,REC ON ONE CARD FORMAT 5D16.6.
C      EK:  NUMBER OF ELECTRONS INVOLVED.
C      TA:  INITIAL TEMPERATURE FOR FREE ENERGY CALCULATIONS.
C      PAS: TEMPERATURE INTERVAL FOR FREE ENERGY CALCULATIONS.
C      RTC:  EXPERIMENTAL ERROR ON TEMPERATURE.
C      REC:  EXPERIMENTAL ERROR ON POTENTIALS.
C
C      TITLE ON ONE CARD FORMAT 19A4.
C
C      FOR EACH OF THE N DATA POINTS:
C      M:  NUMBER OF TEMPERATURE AND EMF VALUES TO BE PROCESSED TO OBTAIN A
C      COUPLE OF AVERAGE VALUES FOR ONE POINT, ON ONE CARD FORMAT I6.
C      M TEMPERATURE-EMF COUPLES OF VALUES PUT IN ARRAYS TC AND EC ON M CARDS
C      FORMAT 2D16.6.
C
C      TO:  ARRAY WHERE P REFERENCE TEMPERATURES ARE PUT, ON P CARDS FORMAT D16.6.
C
C      OUTPUT.
C
C      TITLE,EK.
C
C      TABLE OF AVERAGE TEMPERATURES AND EMFS FOR THE N DATA POINTS, WITH STAN-
C      -DARD DEVIATIONS.
C
C      VALUES OF INTERCEPTS AT DIFFERENT TO'S AND SLOPE OF TEMPERATURE-EMF
C      STRAIGHT LINE, WITH STANDARD DEVIATIONS ON ALL THESE QUANTITIES.

```



```

C
C
C VALUES OF FREE ENERGY AT DIFFERENT T0'S, ENTROPY, ENTHALPY, WITH STANDARD
C DEVIATIONS ON ALL THESE QUANTITIES.
C
C
C TABLE OF Q VALUES OF FREE ENERGY, FROM TA TO TA + Q TIMES PAS.
C
C .....
C
C      IMPLICIT REAL*8(A-H,O-Z)
C      INTEGER P,Q
C      REAL*8 TC(10),EC(10),T(10),E(10),RT(10),RE(10),TO(5),GO(5),RG(5)
C      REAL TITLE(10)
C
C
C CON:  CONVERSION FACTOR FROM EMES TO FREE ENERGIES, EMES IN VOLTS, ALL
C THERMODYNAMIC QUANTITIES IN CALORIES AND DEGREES C.
C
C      DATA CON/0.23054,15398405/
C
C PRELIMINARY READING OF DATA.
C
C      1 READ(5,100,END=9)  N,P,Q,EK,TA,PAS,RTC,PFC,TITLE
C      WRITE(6,101) TITLE,EK
C      WRITE(6,102)
C
C
C LOOP READS TEMPERATURE-EMF DATA FOR N SETS OF M VALUES, AVERAGES THESE,
C AND WRITES M COUPLES OF AVERAGE VALUES WITH STANDARD DEVIATIONS.
C
C      DO 3 I=1,N

```

```

ISN 0002
ISN 0003
ISN 0004
ISN 0005

```

```

ISN 0006

```

```

ISN 0007
ISN 0008
ISN 0009

```

```

ISN 0010

```



```

ISN 0011 READ(5,102) M
ISN 0012 DO 2 J=1,M
ISN 0013 2 READ(5,104) TC(J),EC(J)
ISN 0014 CALL AVERT(M,TC,TS,PTS,RTC)
ISN 0015 T(I)=TS
ISN 0016 RT(I)=RTS
ISN 0017 CALL AVERT(M,EC,ES,PES,REC)
ISN 0018 F(I)=ES
ISN 0019 RE(I)=PES
ISN 0020 2 WRITE(6,105) T(I),RT(I),E(I),RE(I)
C
C LINEAR TEMPERATURE DEPENDENCE OF FMES IS ESTABLISHED BY LEAST-SQUARE
C ANALYSIS. INTERCEPTS ARE CALCULATED FOR SEVERAL ORIGINS. RESULTS ARE
C WRITTEN.
C FREE ENERGY IS CALCULATED AT SEVERAL REFERENCE TEMPERATURES AND IS
C WRITTEN. ENTHALPY AND ENTHALPY ARE CALCULATED AND WRITTEN. STANDARD DEVI-
C -TIONS ARE CALCULATED AND WRITTEN.
C
WRITE(6,106)
DO 6 I=1,P
READ(5,107) TO(I)
IF(I.GT.1) GO TO 4
CALL LEAST(N,T,F,TO(I),A,R,RA,RR)
4 CALL LEAST1(N,T,F,TO(I),B,RR)
WRITE(6,108) TO(I),R,RR
IF(TO(I).EQ.-0.2731603) GO TO 5
GO(I)=-EK*CON*B
RG(I)=EK*CON*PB
5 IF(TO(I).NE.-0.2731603) GO TO 6

```



```

15N 0035
15N 0036
15N 0037
15N 0038
15N 0039
15N 0040
15N 0041
15N 0042
15N 0043
15N 0045
15N 0046
15N 0047

```

```

H=EK*CON*B
RH=EK*CON*B
6 CONTINUE
WRITE(6,109) A,RA
S=EK*CON*A
RS=EK*CON*RA
WRITE(6,110)
DO 7 J=1,P
IF(TO(I),FO,-0.2731603) GO TO 7
WRITE(6,111) TO(I),GO(I),RG(I)
7 CONTINUE
WRITE(6,112) S,RS,H,RH

```

```

C
C LOOP CALCULATES AND WRITES FREE ENERGIES AS A FUNCTION OF TEMPERATURE.
C

```

```

15N 0048
15N 0049
15N 0050
15N 0051
15N 0052
15N 0053
15N 0054
15N 0055

```

```

TP=0.000
GA=H-(TA+0.2731603)*S
WRITE(6,113)
DO 8 I=1,Q
G=GA-TO*S
WRITE(6,114) TA,G
TA=TA+PAS
8 TP=TP+PAS

```

```

C
C CONTROL IS TRANSFERRED TO STATEMENT 1 FOR ANOTHER PROBLEM TO BE TREATED.
C

```



```

ISN 0056      GO TO 1
ISN 0057      9 STOP
ISN 0058      100 FORMAT(3I6/5D16.6/10A4)
ISN 0059      101 FORMAT(1H1,19A4/ , NUMBER OF ELECTRONS INVOLVED= ',D16.6)
ISN 0060      102 FORMAT(1H /// , TEMPERATURE S. D. ON TEMP. MEASURED EMF
              ' S. D. ON EMF ')
ISN 0061      103 FORMAT(16)
ISN 0062      104 FORMAT(2D16.6)
ISN 0063      105 FORMAT(4D16.6)
ISN 0064      106 FORMAT(1H /// , TEMPERATURE DEPENDENCE OF EMF ')
ISN 0065      107 FORMAT(D16.6)
ISN 0066      108 FORMAT(' T0= ',D16.6, ' EMF AT T0= ',D16.6/ , STANDARD DEVIATION O
              'N EMF= ',D16.6)
ISN 0067      109 FORMAT(' , TEMPERATURE COEFF. OF EMF= ',D16.6/ , STANDARD DEVIATION
              ' ON TEMPERATURE COEFF.= ',D16.6)
ISN 0068      110 FORMAT(1H /// , THERMODYNAMIC FUNCTIONS AT REFERENCE TEMPERATURES
              ' ')
ISN 0069      111 FORMAT(' , T0= ',D16.6, ' FREE ENERGY AT T0= ',D16.6/ , STANDARD DE
              'VIATION ON FREE ENERGY= ',D16.6)
ISN 0070      112 FORMAT(' , ENTROPY= ',D16.6/ , STANDARD DEVIATION ON ENTROPY= ',D16.6
              ' / , ENTHALPY= ',D16.6/ , STANDARD DEVIATION ON ENTHALPY= ',D16.6)
ISN 0071      113 FORMAT(1H /// , CALCULATION OF FREE ENERGIES AS A FUNCTION OF TEMP
              'ERATURE /// , TEMPERATURE FREE ENERGY ')
ISN 0072      114 FORMAT(2D16.6)
ISN 0073      END

```

***** END OF COMPILE *****

VI-3. SUBROUTINE 'AVERT' (averaging of data)

```

C .....
C SUBROUTINE AVERT.
C .....
C PURPOSE.
C .....
C SUBROUTINE AVERAGES M VALUES OF A QUANTITY PUT IN ARRAY TC, AND GIVES
C STANDARD DEVIATION ON MEAN VALUE.
C .....
C INPUT.
C .....
C VALUE OF M.
C M VALUES IN ARRAY TC.
C ERS: VALUE OF EXPERIMENTAL ERROR, TO REPLACE STANDARD DEVIATION IF THIS
C IS FOUND TO BE 0.
C .....
C OUTPUT.
C .....
C MEAN VALUE TS.
C STANDARD DEVIATION ON TS, ERT.
C .....
C .....

```



```

ISN 0002      SUBROUTINE AVEPT(M,TC,TS,EPT,ERS)
ISN 0003      IMPLICIT REAL*8(A-H,O-Z)
ISN 0004      REAL*8 TC(20)

C
C  LOOP CALCULATES SUM OF M VALUES OF TC.
C
ISN 0005      SIGMA=0.000
ISN 0006      DO 1 I=1,M
ISN 0007      1 SIGMA=SIGMA+TC(I)

C  MEAN VALUE IS CALCULATED.
C
ISN 0008      TS=SIGMA/DELOAT(M)

C  IF M IS 1 CALCULATION NOT APPLICABLE AND EPT SET TO ERS.
C
ISN 0009      IF(M.LT.2) GO TO 3

C  LOOP CALCULATES SUM OF SQUARE DEVIATIONS.
C
ISN 0011      SIGMA=0.000
ISN 0012      DO 2 I=1,M
ISN 0013      2 SIGMA=SIGMA+(TC(I)-TS)**2

C  STANDARD DEVIATION IS CALCULATED.
C
ISN 0014      EPT=DSQRT(SIGMA/DELOAT(M-1))

C  IF STANDARD DEVIATION FOUND TO BE 0,EPT IS GIVEN THE VALUE OF ERS.
C
ISN 0015      IF(EPT.EQ.0.000) GO TO 3
ISN 0017      RETURN
ISN 0018      EPT=ERS
ISN 0019      RETURN
ISN 0020      END

```

***** END OF COMPIATION *****

VI-4. SUBROUTINE 'LEAST' (linear least squares)

```

C .....
C
C SUBROUTINE LEAST.
C
C PURPOSE.
C SUBROUTINE CALCULATES SLOPE AND INTERCEPT OF THE BEST STRAIGHT LINE
C PASSING THROUGH N POINTS WHOSE ABSCISSAS ARE PUT IN ARRAY X AND ORDINATES
C IN ARRAY Y BY LEAST SQUARE ANALYSIS. CALCULATION IS DONE WITH X0 AS ORIGIN
C FOR X'S. ENTRY LEAST1 ENABLES ONE TO DO ONLY CALCULATION OF SLOPE IF DE-
C -STED.
C
C INPUT.
C
C N AND N COUPLES OF VALUES IN ARRAYS X AND Y.
C X0: ORIGIN FOR X'S.
C
C OUTPUT.
C
C A: SLOPE (NO OUTPUT IF ENTRY LEAST1).
C B: INTERCEPT WITH X=X0.
C T: STANDARD DEVIATION ON INTERCEPT WITH X=X0.
C
C REMARK.
C
C SUBROUTINE USE IS MEANINGLESS FOR N=1. MAINLINE SHOULD AVOID CALLING IT
C IN THAT CASE.
C .....
C

```



```

15N 0003      SUBROUTINE LEAST(N,X,Y,X0,A,R,S,T)
15N 0004      IMPLICIT REAL*8(A-H,O-Z)
15N 0005      REAL*8 X(20),X1(20),Y(20)
15N 0006      INTEGER CPT
15N 0007      CPT=0
15N 0008      GO TO 1
15N 0009      ENTRY LEAST1(N,X,Y,X0,R,T)
15N 0010      CPT=1
15N 0011      1 SX=0.000
15N 0012      SXX=0.000
15N 0013      SXY=0.000
15N 0014      SY=0.000
15N 0015      DO 2 I=1,N
15N 0016      X1(I)=X(I)-X0
15N 0017      SX=SX+X1(I)
15N 0018      SXX=SXX+X1(I)*X1(I)
15N 0019      SXY=SXY+X1(I)*Y(I)
15N 0020      2 SY=SY+Y(I)
15N 0021      C LINEAR EQUATIONS GIVING A AND R ARE SOLVED.
15N 0022      DELTA=SXX*DFLOAT(N)-SX*SX

```



```

ISN 0021      IF(NPT, EQ, 0) A=(SXY*DELNAT(N)-SX*SY)/DELTA
ISN 0022      R=(SXX*SY-SXY*SX)/DELTA

C IF N LESS THAN 3 CALCULATION OF STANDARD DEVIATIONS NOT APPLICABLE AND
C THESE ARE SET TO 0.
C
      IF(N, LT, 3) GO TO 4
      SIGMA=0.000
      DO 3 I=1, N
        SIGMA=SIGMA+(Y(I)-A*X1(I)-B)**2
3      SIGMA=SIGMA+(Y(I)-A*X1(I)-B)**2
C
C CALCULATIONS OF S AND T.
C
      IF(NPT, EQ, 0) S=DSORT(SIGMA*DELNAT(N)/(DELTA*DELNAT(N-2)))
      T=DSORT(SXY*SIGMA/(DELTA*DELNAT(N-2)))
      GO TO 5
4      IF(NPT, EQ, 0) S=0.000
      T=0.000
5      RETURN
      END

***** END OF COMPILATION *****

```


VI-5. Output of 'NERNST' Program

STANDARD POTENTIAL OF A LANTHANUM ELECTRODE IN LiCl-KCl VS PLATINUM REF.

RUN NO	1	TEMPERATURE	MOLE FRACTION	LOG MOLE FR.	CORRECTED EMF
		0.4305600 02	0.3845010-02	-0.3412850 01	-0.3042420 01
		0.4305600 02	0.4415780-02	-0.3354090 01	-0.3036020 01
		0.4303800 02	0.5519650-02	-0.3258000 01	-0.3032870 01
		0.4305000 02	0.6623400-02	-0.3178020 01	-0.3028400 01
		0.4305000 02	0.9851770-02	-0.3052070 01	-0.3023000 01
		0.4305000 02	0.1103030-02	-0.2857060 01	-0.3020900 01

TEMPERATURE= 0.4305000 02
 STANDARD DEVIATION ON TEMPERATURE= 0.6572670-01
 STANDARD EMF= -0.2885550 01
 SLOPE= 0.4544000-01
 THEORETICAL SLOPE= 0.4655370-01
 STANDARD DEVIATION ON EMF= 0.3210530-02
 STANDARD DEVIATION ON SLOPE= 0.1032340-01
 NUMBER OF ELECTRONS INVOLVED= 0.30740 01

RUN NO	TEMPERATURE	MOLE FRACTION	LOG MOLE FR.	CORRECTED EME
2	0.4465000 03	0.1341130-02	-0.2872530 01	-0.3038420 01
	0.4465050 03	0.1532010-02	-0.2814480 01	-0.3031770 01
	0.4471700 03	0.1743620-02	-0.2758550 01	-0.3030610 01
	0.4459800 03	0.1015790-02	-0.2717650 01	-0.3028250 01
	0.4460000 03	0.2107380-02	-0.2676260 01	-0.3027280 01
	0.4462000 03	0.2200520-02	-0.2628360 01	-0.3024340 01

TEMPERATURE=	0.4462820 03
STANDARD DEVIATION ON TEMPERATURE=	0.4886990 00
STANDARD EME=	-0.2882800 01
SLOPE=	0.5360410-01
THEORETICAL SLOPE=	0.4750790-01
STANDARD DEVIATION ON EME=	0.6051730-02
STANDARD DEVIATION ON SLOPE=	0.1008860-01
NUMBER OF ELECTRONS INVOLVED=	0.26640 01

RUN NO	TEMPERATURE	MOLE FRACTION	LOG MOLE FR.	CORRECTED EMF
3	0.4479400 03	0.5021600-02	-0.2299150 01	-0.3051920 01
	0.4477500 03	0.6025500-03	-0.2220010 01	-0.3049370 01
	0.4477500 03	0.7029920-03	-0.2153050 01	-0.3046870 01
	0.4497500 03	0.1004090-02	-0.2998220 01	-0.3037150 01
	0.4476200 03	0.1211270-02	-0.2916760 01	-0.3031830 01
	0.4472500 03	0.1405640-02	-0.2852120 01	-0.3030730 01
	0.4472500 03	0.1606420-02	-0.2794140 01	-0.3023230 01
	0.4470000 03	0.1819620-02	-0.2740020 01	-0.3022660 01
	0.4468000 03	0.2008420-02	-0.2697140 01	-0.3020110 01
	0.4468000 03	0.2208990-02	-0.2655810 01	-0.3020110 01
	0.4468000 03	0.2409800-02	-0.2618020 01	-0.3017610 01

TEMPERATURE=	0.4474280 03
STANDARD DEVIATION ON TEMPERATURE=	0.6069400 00
STANDARD EMF=	-0.2876860 01
SLOPE=	0.5241040-01
THERMODYNAMIC SLOPE=	0.4767270-01
STANDARD DEVIATION ON EMF=	0.1950090-02
STANDARD DEVIATION ON SLOPE=	0.5706280-02
NUMBER OF ELECTRONS INVOLVED=	0.26780 01

RUN NO 4

TEMPERATURE	MOLE FRACTION	LOG MOLE FR.	CORRECTED EMF
0.4508000 02	0.4051850-03	-0.3302350 01	-0.3032560 01
0.4507500 03	0.4630320-03	-0.3334390 01	-0.3020540 01
0.4506000 03	0.5787850-03	-0.3237480 01	-0.3026000 01
0.4502600 03	0.6948150-03	-0.3158130 01	-0.3022890 01
0.4504000 03	0.5260070-03	-0.3033300 01	-0.3017440 01
0.4500000 03	0.1157490-02	-0.3036480 01	-0.3014810 01

TEMPERATURE= 0.4504680 03
 STANDARD DEVIATION ON TEMPERATURE= 0.3070220 00
 STANDARD EMF= -0.2805020 01
 SLOPE= 0.4054530-01
 THEORETICAL SLOPE= 0.4787480-01
 STANDARD DEVIATION ON EMF= 0.1985040-02
 STANDARD DEVIATION ON SLOPE= 0.6224420-02
 NUMBER OF ELECTRONS INVOLVED= 0.35420 01

RUN NO 5

TEMPERATURE	MOLE FRACTION	LOG MOLE FR.	CORRECTED EMF
0.4787500 02	0.3579650-03	-0.3446160 01	-0.3052740 01
0.4786200 03	0.4092540-03	-0.3388010 01	-0.3048700 01
0.4783800 03	0.5112200-02	-0.3291200 01	-0.3042620 01
0.4787000 03	0.6135000-03	-0.3212120 01	-0.3030220 01
0.4785000 03	0.8181000-03	-0.3037150 01	-0.3032660 01
0.4787000 03	0.1022720-02	-0.3090240 01	-0.3028720 01

TEMPERATURE= 0.4786080 03
 STANDARD DEVIATION ON TEMPERATURE= 0.1420450 00
 STANDARD EMF= -0.2873800 01
 SLOPE= 0.5170450-01
 THEORETICAL SLOPE= 0.4972650-01
 STANDARD DEVIATION ON EMF= 0.1489180-02
 STANDARD DEVIATION ON SLOPE= 0.4024600-02
 NUMBER OF ELECTRONS INVOLVED= 0.28860 01

RUN NO. 5

TEMPERATURE MOLE FRACTION LOG MOLE FR. CORRECTED EMF
0.5452500 03 0.8240620-04 -0.4078800 01 -0.3050440 01

TEMPERATURE= 0.5452500 03
STANDARD DEVIATION ON TEMPERATURE= 0.1000000 00
STANDARD EMF= -0.2828500 01
SLOPE= 0.5414550-01
THEORETICAL SLOPE= 0.5414550-01
STANDARD DEVIATION ON EMF= 0.1489180-02
STANDARD DEVIATION ON SLOPE= 0.5000000-02
NUMBER OF ELECTRONS INVOLVED= 0.30000 01

T0= 0.4500000 03
STANDARD EMF AT T0= -0.2882610 01
STANDARD DEVIATION ON EMF AT T0= 0.3577480-02

T0= 0.0
STANDARD EMF AT T0= -0.3078600 01
STANDARD DEVIATION ON EMF AT T0= 0.4042250-01

T0= -0.2731600 03
STANDARD EMF AT T0= -0.2107570 01
STANDARD DEVIATION ON EMF AT T0= 0.6286840-01

TEMPERATURE COEFFICIENT OF STANDARD EMF= 0.4355440-03
STANDARD DEVIATION ON IT= 0.8637840-04

AVERAGE NUMBER OF ELECTRONS INVOLVED= 0.29600 01
STANDARD DEVIATION ON IT= 0.36210 00

THERMODYNAMICS OF A DILUTE SATURATED LA-ZN ALLOY FROM EME DATA
 NUMBER OF ELECTRONS INVOLVED= 0.300000 01

TEMPERATURE	S. D. ON TEMP.	MEASURED EME	S. D. ON EME
0.445518 03	0.729542 00	0.859464 00	0.274046 03
0.450400 03	0.100000 00	0.847400 00	0.704746 03
0.477762 03	0.106066 00	0.835775 00	0.158114 03
0.485464 03	0.224034 00	0.805200 00	0.230048 03
0.503875 03	0.103120 01	0.801437 00	0.154544 03
0.511132 03	0.127115 01	0.810322 00	0.577250 03
0.523109 03	0.123870 00	0.794700 00	0.185164 03
0.585542 03	0.188103 00	0.747908 00	0.153897 03

TEMPERATURE DEPENDENCE OF EME
 TQ= 0.450000 03 EME AT TQ= 0.850653 00
 STANDARD DEVIATION ON EME= 0.386775 02
 TQ= 0.0 EME AT TQ= 0.119778 01
 STANDARD DEVIATION ON EME= 0.200636 01
 TQ= -0.273160 03 EME AT TQ= 0.140850 01
 STANDARD DEVIATION ON EME= 0.464234 01
 TEMPERATURE COEFF. OF EME= -0.771397 03
 STANDARD DEVIATION ON TEMPERATURE COEFF.= 0.600362 04

THERMODYNAMIC FUNCTIONS AT REFERENCE TEMPERATURES
 TQ= 0.450000 03 FREE ENERGY AT TQ= -0.588330 05
 STANDARD DEVIATION ON FREE ENERGY= 0.267503 03
 TQ= 0.0 FREE ENERGY AT TQ= -0.828414 05
 STANDARD DEVIATION ON FREE ENERGY= 0.207927 04
 ENTROPY= -0.532516 02
 STANDARD DEVIATION ON ENTROPY= 0.415155 01
 ENTHALPY= -0.974149 05
 STANDARD DEVIATION ON ENTHALPY= 0.321075 04

CALCULATION OF FREE ENERGIES AS A FUNCTION OF TEMPERATURE

TEMPERATURE	FREE ENERGY
0.4300000 03	-0.5000020 05
0.4350000 03	-0.5062250 05
0.4400000 03	-0.5036670 05
0.4450000 03	-0.5009900 05
0.4500000 03	-0.5082320 05
0.4550000 03	-0.5056640 05
0.4600000 03	-0.5030970 05
0.4650000 03	-0.5003300 05
0.4700000 03	-0.5076610 05
0.4750000 03	-0.5049940 05
0.4800000 03	-0.5023260 05
0.4850000 03	-0.5066590 05
0.4900000 03	-0.5069910 05
0.4950000 03	-0.5043240 05
0.5000000 03	-0.5016560 05
0.5050000 03	-0.5089880 05
0.5100000 03	-0.5063210 05
0.5150000 03	-0.5036530 05
0.5200000 03	-0.5099860 05
0.5250000 03	-0.5083180 05
0.5300000 03	-0.5056500 05
0.5350000 03	-0.5029830 05
0.5400000 03	-0.5003150 05
0.5450000 03	-0.5076480 05
0.5500000 03	-0.5049800 05
0.5550000 03	-0.5023130 05
0.5600000 03	-0.5096450 05
0.5650000 03	-0.5069770 05
0.5700000 03	-0.5043100 05
0.5750000 03	-0.5016420 05
0.5800000 03	-0.5089750 05
0.5850000 03	-0.5063070 05
0.5900000 03	-0.5036400 05
0.5950000 03	-0.5009720 05
0.6000000 03	-0.5083040 05

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